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Abstract: Simultaneous Rayleigh scattering and OH-PLIF imaging measurements of temperature and OH were used to investigate the properties of turbulent premixed flames, including the nature of the 2D thermal structures and scalar dissipation rate in the Cambridge/Sandia swirling bluff body stabilized flames, with and without the effect of swirl. Swirl creates enhanced turbulence as well as outer flow entrainment, and disrupts the pre-flame zone significantly, whilst the high temperature reaction zone as marked by OH remains relatively intact. In particular, the temperature at the location of maximum OH gradient shows very low variance across the flame region.

The 2D image analysis of OH and temperature shows that the corresponding 2D gradients are aligned up to a distance of half the laminar flame thickness away from the flame front, deviating significantly in the case of swirling flames beyond that region. As in previous investigations in diffusion flames, the mean width of the observed thermal structures increases from 300 to 600 microns near the flame, with a main mode around the laminar flame thermal width in the unswirled case. The correlation between 2D thermal fluctuation gradients and variance extracted from the images shows a direct proportionality, with a slope which agrees well with theory in the region of high turbulence away from the base. At the base of the flame where turbulence is low, the local scalar dissipation becomes a function of the local temperature via the thermal diffusivity.

Scalar dissipation rate and scales in swirling turbulent premixed flames

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2 the local temperature via the thermal diffusivity.

3

4

5 **Keywords:** Turbulent premixed flame; Scalar dissipation rate; Dissipative structures; Swirl
6 burner; 2D Rayleigh scattering

1 **1. Introduction**

2 The rate of turbulent micromixing between hot products and reactants controls the overall
3 rate of heat release per unit volume in a flame [1] [2]. In the limit of fast reactions at high
4 Damköhler number (Da), the reaction rate becomes proportional to the scalar dissipation rate,
5 and the flame thickness becomes much smaller than the turbulent spatial scales. Under this
6 thin flame regime, the assumption is often made that the reaction region remains intact, while
7 the reacting interface is transported and extended by turbulence; the reaction rate becomes
8 proportional to the rate at which the flame front propagates through the mixture. This is
9 expressed via the flame surface density [1] [3] [4], or via the rate of scalar dissipation,
10 characterized by the rate of micromixing of the relevant scalar fluctuation [5] [6] [7] [8]. The
11 mean Favre-averaged scalar dissipation rate of a progress of reaction c , is denoted as
12 $\tilde{\chi}_c = \overline{\rho D \nabla c'' \nabla c''} / \bar{\rho}$, where ρ and D are the mixture density and scalar diffusivity, and the
13 usual notation is used: bars for average, tilde for density averaged and double primes for
14 turbulent fluctuation away from the local Favre mean.

15 Many previous experimental studies have explored the internal structure of premixed
16 turbulent flames, to understand under what conditions the reaction zone structure may be
17 affected by turbulence. A number of studies measured a thickening of the preheating zone
18 (also known as thermal or pre-flame zone) due to enhanced transport caused by structures
19 smaller than the preheating zone [9] [10] [11] [12], whereas others [13] [14] suggest a
20 thinning effect. In references [13] [14], simultaneous OH planar laser-induced fluorescence
21 (PLIF) and Rayleigh scattering imaging were used to show that for Karlovitz (Ka) numbers
22 up to 20, the reaction zone is undisturbed; subsequent studies showed that much higher
23 values are required to disrupt the flame zone [15].

24 Direct numerical simulations of high Ka turbulent flames by Aspden *et al.* [16] and
25 Poludnenko and Oran [17] show that although the pre-flame zone is significantly disrupted,

1 the reaction zone remains rather undisturbed, and that the main effect of turbulence is the
2 wrinkling of the reaction zone. A number of experiments have attempted to connect the
3 effects of turbulence intensity and integral length scale to the behaviour of surrogate scalars,
4 showing for example a widening distribution of intermediates such as formaldehyde with
5 increasing turbulence [1] [18] [19] [20] [21] [22]. A full description of the interaction
6 between turbulence and reaction rate remains a key problem in combustion.

7 Previously, Chen and Bilger [12] combined single-plane measurements of OH and two-
8 plane measurements of temperature to study the structure of turbulent methane, propane and
9 hydrogen Bunsen flames, for Karlovitz numbers of up to 3 in the hydrocarbon flames and 10
10 in hydrogen flames. These measurements quantified the gradients of temperature, scalar
11 dissipation and a number of statistical properties of these Bunsen flames [12]. Frank and
12 Kaiser used similar techniques with higher resolution [23] [24] for measurements of thermal
13 dissipation rate and length scales in diffusion flames. Wang *et al.* [25] [26] analysed the
14 resolution requirements for separating noise from signal in scalar dissipation measurements.

15 The present measurements are based on the same techniques developed by Frank and
16 Kaiser [23] [24] for measurements of thermal dissipation rate and corresponding length scales
17 in diffusion flames. The present imaging measurements address the scalar structures in the
18 swirling, bluff-body stabilized methane V-flames extensively described by Sweeney *et al.*
19 [11], at Ka numbers up to 7. These complement previous measurements in turbulent
20 premixed and stratified flames by Sweeney *et al.* [11] [27] [28] using *line*
21 Raman/Rayleigh/CO-LIF and cross-planar OH-PLIF techniques. The latter provided detailed
22 information on local concentrations of major species and temperature, as well as the local
23 temperature gradients at the flame along a line, and corresponding 3D gradients at the flame
24 front. However, such line measurements cannot offer insight into the detailed structure of
25 mixing and scalar dissipation rate in the flow.

1 In the present work, we use high resolution Rayleigh scattering and OH LIF imaging to
2 measure the 2D length scales of the characteristic structures, as well as the 2D thermal
3 dissipation rate, for the same premixed flames at no swirl and high swirl conditions. The
4 analysis also examines the assumption of alignment between the temperature and OH
5 gradient, used in previous papers [11], and the robustness of the relationship between
6 dissipation rate and variance suggested by turbulent combustion models [6] [29] [30].

7

8 **2. Experimental details**

9 ***2.1. Cambridge/Sandia stratified swirl burner and operating conditions***

10 The geometry of the swirl burner is described in detail in Ref. [28]. Long co-annular tubes
11 ensure that a well-developed turbulent flow is delivered to the flame region. A ceramic
12 central bluff body is used to stabilize the flame with minimal heat loss. Flow through the
13 outer annulus is split between an axial and a swirling flow emerging at the base of the burner,
14 providing a maximum swirl flow ratio (SFR) of 0.33 [28].

15 Imaging measurements were performed at the three locations indicated by the field of
16 view (FOV) regions in Fig. 1. Each field of view is approximately centered at the local mid-
17 point of the flame brush, with dimensions of $24.5 \times 16.3 \text{ mm}^2$ and centreline coordinates as
18 listed in Table 1. A subset of the previously used operating conditions in Ref. [28] is studied
19 in this paper, focusing on comparisons between non-swirling (SFR=0%) and highly swirling
20 (SFR=33%) flames, with no stratification between the inner and outer annuli, with a
21 premixed equivalence ratio of $\phi=0.75$ (Table 2).

22

Case	SFR (%)	S (-)	FOV 1	FOV 2	FOV 3
<i>SwB1</i>	0	0.03	(05, 15)	(08, 30)	(11, 50)
<i>SwB3</i>	33	0.54	(13, 15)	(21, 30)	(27, 50)

23

1 **Table 1.** Operating conditions for the flames considered. The velocity of the inner channel is $U_i = 8.3$
 2 m/s ($Re_i = 5960$) and for the outer channel, $U_o = 18.7$ m/s, ($Re_i = 11500$ based on hydraulic diameter
 3 of the outer annulus) with co-flow velocity $U_{co} = 0.4$ m/s. Coordinates of the center of the FOV in
 4 radial and axial distances from the centreline at the base of the burner, in mm. SFR: ratio of incoming
 5 tangential to total flow rate.

6

Flames	$\frac{U'}{S_L}$			
z (mm)	2	10	30	50
<i>SwB1</i>	11.5	9.7	10.0	9.8
<i>SwB3</i>	31.8	27.5	17.9	12.9

7 **Table 2.** Maximum value of the ratio for the total mean velocity fluctuation U' divided by the
 8 laminar speed S_L for a given axial location, z . Turbulent velocity measurements acquired with laser
 9 Doppler anemometry (LDA) and particle image velocimetry (PIV) by Zhou *et al.* [28].

10

11 **2.2. Optical arrangement**

12 Simultaneous Rayleigh scattering and OH-PLIF imaging measurements were performed
 13 in the Advanced Imaging Laboratory at Sandia National Laboratories. The experimental
 14 arrangement consisted of the high-resolution Rayleigh imaging apparatus described in Ref.
 15 [31], combined with an additional laser/camera system for simultaneous OH-PLIF imaging
 16 [23].

17 A laser sheet (100 μm thickness) used for Rayleigh scattering was produced from a
 18 frequency-doubled Nd:YAG laser, with an energy of 2.0 J/pulse at 532 nm at a repetition rate
 19 of 10 Hz. OH PLIF was excited by the frequency-doubled output of a 10-Hz Nd:YAG-
 20 pumped dye-laser tuned to 283.01 nm to pump the Q₁(6) transition of the A-X(1,0) band of
 21 OH using 1.2 mJ/pulse.

22 Rayleigh scattering from the probe volume was imaged onto an unintensified interline-
 23 transfer CCD camera (SensiCam QE, PCO/Cooke). A second interline-transfer camera was

1 used to image Rayleigh scattering from the air co-flow adjacent to the burner to account for
2 shot-to-shot variations in the laser profile. The Rayleigh scattering from room temperature air
3 was used as a reference signal. The background signal was extracted from measurements in
4 pure air and helium streams which have known Rayleigh scattering cross sections.

5 The expanded laser beams used for Rayleigh scattering and OH-PLIF were overlapped by
6 stacking the beam planes crossing the centreline of the burner along the axial direction. The
7 OH fluorescence emission was imaged onto an intensified CCD camera (Andor DH312T-
8 18H-83). The shot-to-shot laser energy fluctuations of $\pm 2\%$ were negligible for the subsection
9 of the dye-laser beam that was used for PLIF imaging. The OH-PLIF images were corrected
10 for variations in the average dye-laser beam profile. The FOV of the Rayleigh camera was a
11 $19.3 \times 14.6 \text{ mm}^2$ subsection of the $24.5 \times 16.3 \text{ mm}^2$ region imaged by the OH-PLIF camera. The
12 pixel resolution of the Rayleigh scattering measurement was $14 \mu\text{m}/\text{pixel}$. The resolution of
13 the OH-PLIF camera was approximately $140 \mu\text{m}/\text{pixel}$ and was limited by the resolution of
14 the image intensifier.

15 Both OH PLIF images and Rayleigh images were smoothed using a Gaussian filter, with
16 the latter relying on a variable, temperature-dependent kernel as described in [31] [24].
17 Additional information regarding the image processing and system setup are detailed in the
18 relevant references. A fixed Rayleigh scattering cross section equal to 1.09 times that of air
19 was used to determine the temperature for all conditions in Table 1. The maximum
20 uncertainty in the temperature measurement resulting from composition variations was
21 estimated as $\pm 3\text{-}4\%$.

1 **3. Data analysis**

2 Figures 2a and 2b show an example of normalized OH LIF signal and the temperature
3 obtained from the Rayleigh scattering signal, respectively. The flame front location is defined
4 here as the location of the maximum gradient of the OH PLIF signal [32], and is indicated by
5 a black line in the figure. For the present comparisons, this definition provides a well defined
6 reference that is expected to be near the location of peak heat release rate [32]. The local
7 flame normal is defined with respect to the flame front contour, and is shown as white dashed
8 lines in the figure.

9 Local ensemble averaged temperatures $\langle T \rangle$ and the corresponding root mean squared
10 temperature fluctuations $\langle T' \rangle$ are obtained from 2000 individual shots for each FOV. A
11 local flame temperature T_f is defined as the instantaneous temperature at the flame front.
12 Deviations of temperature relative to the instantaneous local flame temperature are defined
13 along the normal coordinate n , as $T'_f = T - T_f$, with corresponding mean and rms values,
14 $\langle T_f \rangle$ and $\langle T'_f \rangle$, respectively.

15 The 2D temperature gradients $\nabla T = \frac{dT}{dr} \mathbf{i} + \frac{dT}{dz} \mathbf{k}$ are determined via first order central
16 differencing after filtering. The gradients of the temperature fluctuations are defined as
17 $\nabla T' = \nabla(T - \langle T \rangle)$. In previous line measurements [11], the 3D temperature gradients
18 throughout the flame were assumed to be parallel to the flame normal obtained from the cross
19 planar OH PLIF measurements. Here we assess the quality of this assumption in 2D by
20 determining the statistics of the angle θ between the temperature and OH gradients as a
21 function of temperature. Further, the characteristic 2D thermal diffusion width, λ_D , of the
22 dissipation layer is obtained from the images. The diffusion width is defined as the full width
23 at 20% of the local maximum temperature gradient, as determined along the direction normal
24 to the layer, which provides a more direct measure of the structure length scale than is
25 possible with 1D measurements [24]. The value of the thermal diffusivity, α , is obtained by

1 interpolating a lookup table of calculated values as a function of temperature from premixed
2 unstrained flames at premixed conditions of $\phi=0.75$.

3

4 **4. Results and discussion**

5

6 **4.1. Single shot measurements**

7 Single shot images of OH PLIF signal, temperature and respective fluctuations for both
8 flow conditions at the regions nearest to the base, FOV1 (bottom panel), and furthest away,
9 FOV3 (top panel), are shown in Fig. 3. For the non-swirling case, SwB1, a comparison of the
10 temperature and OH PLIF images shows that the overall topologies of the OH-PLIF images
11 are well aligned with the temperature images, even in the furthest downstream regions where
12 turbulence is more developed. The flame front contour (location of the highest gradient OH
13 signal) overlaps almost exactly with an isotherm at approximately 1450 K throughout the
14 flame region, with a thermal thickness that is only slightly larger than the laminar flame
15 thickness of $\delta_L = 588 \mu\text{m}$ calculated for $\phi=0.75$.

16 Contrast this behavior with the swirling case, SwB3 (Fig. 3, right), in which the pre-
17 heating region is highly disrupted and convoluted, particularly in the region further
18 downstream (FOV3): regions of high temperature appear in the reactant region, which could
19 be a result of out-of-plane motion of neighboring regions of the flame, as well as entrainment
20 of the flame structures into the reaction zone. The product temperatures are lower than in
21 SwB1 as a result of the swirl-induced entrainment of co-flow air into the central product zone
22 [11] [28]. The OH PLIF signal boundary and the corresponding flame contour is significantly
23 distorted but not dispersed throughout the pre-heating zone. Although the OH radical is not a
24 definitive marker of the flame location under all conditions, the distribution of the OH PLIF

1 signal is very different from that of the temperature. For temperatures above 1200 K, there
2 are no clearly detectable thermal structures.

3 The third row in each panel of Fig. 3 shows the instantaneous fluctuation, T' , relative to
4 the local mean temperature for the two regions FOV 1 and FOV 3. The highest deviations
5 from the mean temperature straddle the location of the flame, as expected.

6

7 **4.2. Flame temperature statistics**

8 Figure 4 shows ensemble mean temperatures and rms fluctuations along the coordinate
9 normal to the flame, n , where $n=0$ is the flame front defined as the location of maximum
10 gradient in the OH LIF signal. The variance is lowest at $n=0$, increases to a maximum away
11 from the flame front, and eventually decreases to zero in the products and reactants. Laminar
12 unstrained premixed flame simulations at $\phi=0.75$ (based on GRI Mech 3.0 [33] and full
13 transport properties) are also shown. The measured maximum conditional mean temperatures
14 in the present dataset appear to be systematically lower than the calculated adiabatic flame
15 temperature (which agrees well with the line measurements in [11]), by 150 K in the non-
16 swirl case. The sources of the discrepancies are unclear, as all calibrations and procedures
17 have been checked.

18 The mean product temperature in the swirling case SwB3 is lower than the corresponding
19 non-swirling case SwB1 owing to entrainment. The fluctuation in temperature is significantly
20 increased by the addition of swirl, particularly in the pre-flame region, due to entrainment of
21 air, both around the outer edges of the flame, as well as through the top in the open
22 recirculation zone [11] [28]. The low fluctuation in temperature at the flame front shows that
23 the location of peak OH gradient, and presumably the reaction zone, is tied to a particular
24 temperature, indicating that the flames appear as curved and strained flamelets.

25

1 ***4.3. Temperature and OH 2D gradient alignment***

2 Since temperature and OH are the most easily imaged scalars, these are often used as
3 surrogates for progress of reaction markers [13] [14] [27] [34]. However, it is clear that their
4 behaviour in the present flames can be very different, and that isocontours of temperature do
5 not always align with those of OH LIF signals. In the present study, it is possible to identify,
6 in 2D, how well the isoscalars align around the flame. In particular, in the study using line
7 measurements [11], two-plane OH LIF imaging was used to determine the orientation of the
8 3D flame normal for the flame crossing the measurement line. This orientation was then used
9 to correct the temperature gradient along the measurement line, under the assumption that the
10 OH contour is parallel to the temperature contour in the vicinity of the thermal zone. Figure 5
11 shows how well this assumption holds by evaluating the angle between the normal directions
12 for contours of temperature and OH LIF signal as a function of the flame distance from the
13 flame along its normal divided by the laminar flame thickness, n/δ_L . Near the flame front
14 contour at $n/\delta_L=0$, θ is approximately zero, indicating that the temperature gradients are well
15 aligned with the OH LIF gradients. At distances beyond $\delta_L/2$, the assumption starts to break
16 down as the angle increases.

17

18 ***4.4. Thermal dissipation scales***

19 The propagation of reactions in a flame depends on the effective generation and
20 dissipation of turbulent structures throughout the flame [5] [6], allowing the increase in the
21 mean rate of reaction throughout the flame. The distribution and characteristic width of the
22 structures generally follow that of a passive scalar, but are significantly affected by the local
23 temperatures, which increase the diffusivity and viscosity, thus suppressing turbulence, and
24 increasing length scales. This has been shown to be true in diffusion flames [23] [24]; here
25 we demonstrate the similarities and differences for swirling premixed flames.

1 Instantaneous images of the thermal dissipation structures are shown in Fig. 6: for the
2 non-swirling case (left), the structures are associated primarily with the flame, and evolve
3 slowly as the turbulence develops downstream. For the high swirl case, the structures are
4 widely distributed, owing to the higher turbulence and entrainment of outside air. Yet these
5 structures become thicker towards the product region (towards the right of each image).

6 In Figure 7, the dissipation structures are characterized by considering the probability
7 density functions (pdf) of their width, λ_D , as a function of the temperature across the flames.
8 The pdfs are conditioned to the temperature of the structure, so that the modes are not
9 representative of the overall image, as the integral of each pdf in Fig. 7 is unity. In general,
10 the structures become systematically thicker towards the high temperature regions, owing to
11 the combined effects of dilatation and increasing viscosity with temperature. Beyond 1400 K,
12 detectable structure widths are mostly a result of the noise remaining from the beam steering
13 correction. For the non-swirling flame SwB1, the most probable width of 600 μm appears at
14 1000 K and corresponds closely to the unstrained laminar flame thickness of 588 μm . For the
15 high swirl case SwB3, the PDF of layer widths has a peak around 300 μm at 400 K, arising
16 from the mixing of product and fresh reactants via entrainment. Less frequent, thicker flame
17 structures appear as temperature increases, to values approximating the width of the
18 unstrained laminar flame, as in case SwB1. In case SwB3, the width of the PDF distributions
19 increases with temperature, and the overall unconditioned PDF distribution is significantly
20 broader than in the non-swirl case.

21 Turbulent combustion models rely on the relationship between statistical variances of the
22 gradients of the reaction progress variable that represents micromixing and the average
23 reaction rate. DNS studies have been used to scale and adjust models based on such
24 correlations [5] [6] [7] [8]. Previous models for scalar dissipation suggest a linear
25 correlation between the Favre mean scalar dissipation of the reaction progress variable, $\tilde{\chi}_c$,

1 and the variance of the relevant progress variable, \tilde{c}'' . Specifically, the work by Kolla *et al.*
 2 [30] and references therein based on the original Bray model [35] suggest a specific
 3 correlation for the normalized Favre averaged scalar dissipation of a reaction progress
 4 variable to its variance, with a coefficient of order unity in the ideal case of high Da. Using
 5 temperature as the progress of reaction, normalized by ΔT , the temperature rise for the
 6 adiabatic flame (1622 K for $\phi=0.75$), it is possible to reproduce these quantities (Fig. 8) in
 7 the form of the normalized Favre averaged scalar dissipation $\hat{\chi}_c = \tilde{\chi}_T \tau_f = \frac{\tau_f}{\Delta T \bar{\rho}} <$
 8 $\rho \alpha |\nabla T''|^2$, where $\tau_f = \frac{\delta_L}{S_L}$ is the laminar flame transit time. The laminar flame transit
 9 time and the density were estimated from the temperature measurements, but variations in
 10 mixture composition were neglected. Values for $\hat{\chi}_c$ are plotted as a function of the Favre
 11 averaged normalized variance in temperature as progress of reaction, $\tilde{c}''^2 = \tilde{T}''^2 / \Delta T^2 =$
 12 $\langle (\rho/\bar{\rho}) (T - \tilde{T})^2 \rangle / \Delta T^2$, and colored by the local mean temperature $\langle T \rangle$.

13 The plots in Fig. 8 for FOV1 and FOV2 of SwB1 show two branches, corresponding to
 14 the higher and lower temperature regions of the flame, reflecting the temperature dependence
 15 of the thermal diffusivity. Further away from the base, additional turbulence is generated by
 16 shear at the edges, the slope becomes lower, and the two branches merge. At this limit, the
 17 mean scalar dissipation rate becomes highly correlated with the mean variance in a nearly
 18 linear relationship, indicating that the variations in molecular diffusivity have less of an
 19 influence. The theory and DNS predictions for the relevant constant suggest that the slope of
 20 the curve should scale as [30]:

$$\hat{\chi}_c = \frac{1}{\beta} \left[\left(2 \frac{K_c^*}{\theta_T} - C_4 (1 + Ka)^{-0.4} \right) \theta_T + C_3 (1 + Ka^{-0.5})^{-1} Da^{-1} \right] \tilde{c}''^2$$

21 where θ_T is the ratio of absolute product to reactant temperatures, $Da = \tau_T / \tau_f$ is the
 22 Dahmköhler number and $Ka = \tau_f / \tau_\eta$ the Karlovitz number, τ_T the integral turbulent time

1 scales, τ_η the Kolmogorov time scale, and the remaining quantities are constants. The values
2 of the constants proposed by Kolla *et al.* [30] are approximately $\frac{K_c^*}{\theta_T} = 0.82$ to 0.85, $C_4 =$
3 1.1 , $C_3 = 1.1$ and $\beta = 6.7$, and values for the present mixture are: $\theta_T = 1 + \frac{\Delta T}{T_0} = 6.5$. In the
4 limit of Da and zero Ka, the slope indicated by the model should be 0.53 to 0.58. Higher
5 values of turbulence would in general decrease Da and increase Ka. The measured slopes for
6 SwB3 are closer to the limit model than those of SwB1, with the closest agreement at
7 location FOV3. The higher turbulence levels in SwB3 and at FOV3 are consistent with the
8 closer match to the theory. On the other hand, for SwB3 there is significant entrainment and
9 mixing, so that one would expect a departure between the correlation between variance and
10 dissipation. Further work connecting the present measurements to local turbulent velocity
11 measurements should enlighten the correlation between theory, experiments and correlations
12 extracted from DNS calculations.

13
14

15 **Conclusions**

16 The present investigation showed how swirl and the ensuing high turbulence and
17 entrainment significantly disrupt the flame thermal zone in a premixed flame, whilst the high
18 temperature reaction zone interface, as marked by the OH contour, remains relatively intact.
19 The temperature at which the maximum OH gradient appears remains relatively unchanged,
20 showing the lowest variance across the flame region, and coinciding with an isocontour of
21 about 1450 K. In support of previous assumptions regarding the alignment of OH and
22 temperature contours, the present experiments showed that indeed, the 2D gradients of OH
23 and temperature align well, up to a distance of about one half the laminar flame thickness
24 away from the flame front, with significant deviations beyond that region in the case of
25 swirling flames.

1 Similarly to previous investigations of diffusion flames, characteristic diffusive widths of
2 the observed thermal structures vary from 300 to 600 microns, from the non-reacting to the
3 higher temperature regions, as a consequence of dilatation and increasing viscosity. The most
4 probable structure widths coincide with the laminar flame thickness in the unswirled, whilst a
5 more uniform distribution of widths appears in the latter case, with a peak at around 400 K
6 temperatures, corresponding to mixing of product and fresh reactants.

7 The Favre-averaged 2D scalar dissipation obtained from the temperature gradients
8 correlates well with the measured variance in the high turbulence regions. In the low
9 turbulence region near the base, the value of the scalar dissipation is not monotonic with the
10 variance of the progress variable and the local temperature. Future work should target
11 understanding the details of these correlations based on the local turbulent velocity
12 characteristics.

13

14

15 **Acknowledgements**

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Figure Captions

Figure 1. Left half: schematic indicating FOV locations for distances above the burner surface. Streamlines and absolute velocity for SwB1 (left half) and SwB3 (right half). Rectangles represent the imaging locations [28].

Figure 2. An example of flame normal extracted from single shot profiles of OH-PLIF. (a) Instantaneous image of normalized OH LIF intensity, (b) temperature field (in K), overlaid with the flame front at the maximum gradient location (black line) and corresponding flame normal (white lines).

Figure 3. Single shot images of normalized OH LIF signal (top rows), temperature (middle rows) in K, and temperature fluctuation, T' , relative to the ensemble averaged temperature field, in K (bottom row) for no swirl (left) and high swirl (right). Top panel: FOV3, bottom: FOV1.

Figure 4: Mean (blue line) and rms (blue bars) fluctuation profiles of the temperature, for FOV1-3 along the normal coordinate n , where zero is the flame front. Black lines denote the unstrained laminar flame values for $\phi = 0.75$.

Figure 5. Scatter plot of normalized angle (in multiples of π) between the normal directions for contours of temperature and OH as a function of the absolute value of the normalized distance from the flame front, coloured by a temperature index defined as $\Omega = (T - T_o)/(T_{f,0} - T_o)$, where $T_{f,0}$ represents the unstrained laminar flame temperature at the location of maximum gradient of OH at equivalence ratio of 0.75. Magenta lines represent the mean and rms values.

Figure 6. Instantaneous temperature fluctuation gradients for SwB1 and SwB3. Bottom to top: FOV1 to 3. The right hand side of the figure is the product side.

Figure 7. Conditioned probability density functions of λ_D widths conditioned on temperature over a 20 K range.

Figure 8. Scatter plots of normalized Favre-averaged scalar dissipation rate, $\tilde{\chi}_c$, and mean Favre variance of progress variable temperature variance, $\widetilde{c''^2}$, colored by the corresponding mean local temperature. The SDR is normalized by the term (δ_L/S_L) ; where S_L is the laminar flame speed of the methane/air flame ($S_L = 0.214$ m/s) and δ_L is the laminar flame thickness ($\delta_L = 0.588$ mm) derived from laminar flame calculations at an equivalence ratio of $\phi = 0.75$. The figures quoted on each panel are the slopes of each correlation.

Table Captions

Table 1. Operating conditions. The velocity of the inner channel is $U_i = 8.3$ m/s ($Re_i = 5960$) and for the outer channel, $U_o = 18.7$ m/s, ($Re_i = 11500$ based on hydraulic diameter of the outer annulus) with co-flow velocity $U_{co} = 0.4$ m/s. Coordinates of the center of the FOV in radial and axial distances from the centreline at the base of the burner, in mm. SFR: ratio of incoming tangential to total flow rate.

Table 2. Maximum value of the ratio for the total mean velocity fluctuation U' divided by the laminar speed S_L for a given axial location, z . Turbulent velocity measurements acquired with laser Doppler anemometry (LDA) and particle image velocimetry (PIV) by Zhou *et al.* [28].

Scalar dissipation rate and scales in swirling turbulent premixed flames

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1 **Scalar dissipation rate and scales in swirling turbulent premixed flames**

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8
9
10 **Abstract**

11 Simultaneous Rayleigh scattering and OH-PLIF imaging measurements of temperature
12 and OH were used to investigate the properties of turbulent premixed flames, including the
13 nature of the 2D thermal structures and scalar dissipation rate in the Cambridge/Sandia
14 swirling bluff body stabilized flames, with and without the effect of swirl. Swirl creates
15 enhanced turbulence as well as outer flow entrainment, and disrupts the pre-flame zone
16 significantly, whilst the high temperature reaction zone as marked by OH remains relatively
17 intact. In particular, the temperature at the location of maximum OH gradient shows very low
18 variance across the flame region.

20 The 2D image analysis of OH and temperature shows that the corresponding 2D
21 gradients are aligned up to a distance of half the laminar flame thickness away from the flame
22 front, deviating significantly in the case of swirling flames beyond that region. As in previous
23 investigations in diffusion flames, the mean width of the observed thermal structures
24 increases from 300 to 600 microns near the flame, with a main mode around the laminar
25 flame thermal width in the unswirled case. The correlation between 2D thermal fluctuation
26 gradients and variance extracted from the images shows a direct proportionality, with a slope
27 which agrees well with theory in the region of high turbulence away from the base. At the

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1 base of the flame where turbulence is low, the local scalar dissipation becomes a function of
2 the local temperature via the thermal diffusivity.

3

4

5 **Keywords:** Turbulent premixed flame; Scalar dissipation rate; Dissipative structures; Swirl
6 burner; 2D Rayleigh scattering

1 **1. Introduction**

2 The rate of turbulent micromixing between hot products and reactants controls the overall
3 rate of heat release per unit volume in a flame [1] [2]. In the limit of fast reactions at high
4 Damköhler number (Da), the reaction rate becomes proportional to the scalar dissipation rate,
5 and the flame thickness becomes much smaller than the turbulent spatial scales. Under this
6 thin flame regime, the assumption is often made that the reaction region remains intact, while
7 the reacting interface is transported and extended by turbulence; the reaction rate becomes
8 proportional to the rate at which the flame front propagates through the mixture. This is
9 expressed via the flame surface density [1] [3] [4], or via the rate of scalar dissipation,
10 characterized by the rate of micromixing of the relevant scalar fluctuation [5] [6] [7] [8]. The
11 mean Favre-averaged scalar dissipation rate of a progress of reaction c , is denoted as
12 $\tilde{\chi}_c = \overline{\rho D \nabla c'' \nabla c''} / \bar{\rho}$, where ρ and D are the mixture density and scalar diffusivity, and the
13 usual notation is used: bars for average, tilde for density averaged and double primes for
14 turbulent fluctuation away from the local Favre mean.

15 Many previous experimental studies have explored the internal structure of premixed
16 turbulent flames, to understand under what conditions the reaction zone structure may be
17 affected by turbulence. A number of studies measured a thickening of the preheating zone
18 (also known as thermal or pre-flame zone) due to enhanced transport caused by structures
19 smaller than the preheating zone [9] [10] [11] [12], whereas others [13] [14] suggest a
20 thinning effect. In references [13] [14], simultaneous OH planar laser-induced fluorescence
21 (PLIF) and Rayleigh scattering imaging were used to show that for Karlovitz (Ka) numbers
22 up to 20, the reaction zone is undisturbed; subsequent studies showed that much higher
23 values are required to disrupt the flame zone [15].

24 Direct numerical simulations of high Ka turbulent flames by Aspden *et al.* [16] and
25 Poludnenko and Oran [17] show that although the pre-flame zone is significantly disrupted,

1 the reaction zone remains rather undisturbed, and that the main effect of turbulence is the
2 wrinkling of the reaction zone. A number of experiments have attempted to connect the
3 effects of turbulence intensity and integral length scale to the behaviour of surrogate scalars,
4 showing for example a widening distribution of intermediates such as formaldehyde with
5 increasing turbulence [1] [18] [19] [20] [21] [22]. A full description of the interaction
6 between turbulence and reaction rate remains a key problem in combustion.

7 Previously, Chen and Bilger [12] combined single-plane measurements of OH and two-
8 plane measurements of temperature to study the structure of turbulent methane, propane and
9 hydrogen Bunsen flames, for Karlovitz numbers of up to 3 in the hydrocarbon flames and 10
10 in hydrogen flames. These measurements quantified the gradients of temperature, scalar
11 dissipation and a number of statistical properties of these Bunsen flames [12]. Frank and
12 Kaiser used similar techniques with higher resolution [23] [24] for measurements of thermal
13 dissipation rate and length scales in diffusion flames. Wang *et al.* [25] [26] analysed the
14 resolution requirements for separating noise from signal in scalar dissipation measurements.

15 The present measurements are based on the same techniques developed by Frank and
16 Kaiser [23] [24] for measurements of thermal dissipation rate and corresponding length scales
17 in diffusion flames. The present imaging measurements address the scalar structures in the
18 swirling, bluff-body stabilized methane V-flames extensively described by Sweeney *et al.*
19 [11], at Ka numbers up to 7. These complement previous measurements in turbulent
20 premixed and stratified flames by Sweeney *et al.* [11] [27] [28] using *line*
21 Raman/Rayleigh/CO-LIF and cross-planar OH-PLIF techniques. The latter provided detailed
22 information on local concentrations of major species and temperature, as well as the local
23 temperature gradients at the flame along a line, and corresponding 3D gradients at the flame
24 front. However, such line measurements cannot offer insight into the detailed structure of
25 mixing and scalar dissipation rate in the flow.

1 In the present work, we use high resolution Rayleigh scattering and OH LIF imaging to
2 measure the 2D length scales of the characteristic structures, as well as the 2D thermal
3 dissipation rate, for the same premixed flames at no swirl and high swirl conditions. The
4 analysis also examines the assumption of alignment between the temperature and OH
5 gradient, used in previous papers [11], and the robustness of the relationship between
6 dissipation rate and variance suggested by turbulent combustion models [6] [29] [30].

7

8 **2. Experimental details**

9 ***2.1. Cambridge/Sandia stratified swirl burner and operating conditions***

10 The geometry of the swirl burner is described in detail in Ref. [28]. Long co-annular tubes
11 ensure that a well-developed turbulent flow is delivered to the flame region. A ceramic
12 central bluff body is used to stabilize the flame with minimal heat loss. Flow through the
13 outer annulus is split between an axial and a swirling flow emerging at the base of the burner,
14 providing a maximum swirl flow ratio (SFR) of 0.33 [28].

15 Imaging measurements were performed at the three locations indicated by the field of
16 view (FOV) regions in Fig. 1. Each field of view is approximately centered at the local mid-
17 point of the flame brush, with dimensions of $24.5 \times 16.3 \text{ mm}^2$ and centreline coordinates as
18 listed in Table 1. A subset of the previously used operating conditions in Ref. [28] is studied
19 in this paper, focusing on comparisons between non-swirling (SFR=0%) and highly swirling
20 (SFR=33%) flames, with no stratification between the inner and outer annuli, with a
21 premixed equivalence ratio of $\phi=0.75$ (Table 2).

22

Case	SFR (%)	S (-)	FOV 1	FOV 2	FOV 3
<i>SwB1</i>	0	0.03	(05, 15)	(08, 30)	(11, 50)
<i>SwB3</i>	33	0.54	(13, 15)	(21, 30)	(27, 50)

23

1 **Table 1.** Operating conditions for the flames considered. The velocity of the inner channel is $U_i = 8.3$
2 m/s ($Re_i = 5960$) and for the outer channel, $U_o = 18.7$ m/s, ($Re_i = 11500$ based on hydraulic diameter
3 of the outer annulus) with co-flow velocity $U_{co} = 0.4$ m/s. Coordinates of the center of the FOV in
4 radial and axial distances from the centreline at the base of the burner, in mm. SFR: ratio of incoming
5 tangential to total flow rate.

6

Flames	$\frac{U'}{S_L}$			
z (mm)	2	10	30	50
<i>SwB1</i>	11.5	9.7	10.0	9.8
<i>SwB3</i>	31.8	27.5	17.9	12.9

7 **Table 2.** Maximum value of the ratio for the total mean velocity fluctuation U' divided by the
8 laminar speed S_L for a given axial location, z . Turbulent velocity measurements acquired with laser
9 Doppler anemometry (LDA) and particle image velocimetry (PIV) by Zhou *et al.* [28].

10

11 **2.2. Optical arrangement**

12 Simultaneous Rayleigh scattering and OH-PLIF imaging measurements were performed
13 in the Advanced Imaging Laboratory at Sandia National Laboratories. The experimental
14 arrangement consisted of the high-resolution Rayleigh imaging apparatus described in Ref.
15 [31], combined with an additional laser/camera system for simultaneous OH-PLIF imaging
16 [23].

17 A laser sheet (100 μm thickness) used for Rayleigh scattering was produced from a
18 frequency-doubled Nd:YAG laser, with an energy of 2.0 J/pulse at 532 nm at a repetition rate
19 of 10 Hz. OH PLIF was excited by the frequency-doubled output of a 10-Hz Nd:YAG-
20 pumped dye-laser tuned to 283.01 nm to pump the Q₁(6) transition of the A-X(1,0) band of
21 OH using 1.2 mJ/pulse.

22 Rayleigh scattering from the probe volume was imaged onto an unintensified interline-
23 transfer CCD camera (SensiCam QE, PCO/Cooke). A second interline-transfer camera was

1 used to image Rayleigh scattering from the air co-flow adjacent to the burner to account for
2 shot-to-shot variations in the laser profile. The Rayleigh scattering from room temperature air
3 was used as a reference signal. The background signal was extracted from measurements in
4 pure air and helium streams which have known Rayleigh scattering cross sections.
5 The expanded laser beams used for Rayleigh scattering and OH-PLIF were overlapped by
6 stacking the beam planes crossing the centreline of the burner along the axial direction. The
7 OH fluorescence emission was imaged onto an intensified CCD camera (Andor DH312T-
8 18H-83). The shot-to-shot laser energy fluctuations of $\pm 2\%$ were negligible for the subsection
9 of the dye-laser beam that was used for PLIF imaging. The OH-PLIF images were corrected
10 for variations in the average dye-laser beam profile. The FOV of the Rayleigh camera was a
11 $19.3 \times 14.6 \text{ mm}^2$ subsection of the $24.5 \times 16.3 \text{ mm}^2$ region imaged by the OH-PLIF camera. The
12 pixel resolution of the Rayleigh scattering measurement was $14 \mu\text{m}/\text{pixel}$. The resolution of
13 the OH-PLIF camera was approximately $140 \mu\text{m}/\text{pixel}$ and was limited by the resolution of
14 the image intensifier.

15 Both OH PLIF images and Rayleigh images were smoothed using a Gaussian filter, with
16 the latter relying on a variable, temperature-dependent kernel as described in [31] [24].
17 Additional information regarding the image processing and system setup are detailed in the
18 relevant references. A fixed Rayleigh scattering cross section equal to 1.09 times that of air
19 was used to determine the temperature for all conditions in Table 1. The maximum
20 uncertainty in the temperature measurement resulting from composition variations was
21 estimated as $\pm 3\text{-}4\%$.

1 **3. Data analysis**

2 Figures 2a and 2b show an example of normalized OH LIF signal and the temperature
3 obtained from the Rayleigh scattering signal, respectively. The flame front location is defined
4 here as the location of the maximum gradient of the OH PLIF signal [32], and is indicated by
5 a black line in the figure. For the present comparisons, this definition provides a well defined
6 reference that is expected to be near the location of peak heat release rate [32]. The local
7 flame normal is defined with respect to the flame front contour, and is shown as white dashed
8 lines in the figure.

9 Local ensemble averaged temperatures $\langle T \rangle$ and the corresponding root mean squared
10 temperature fluctuations $\langle T' \rangle$ are obtained from 2000 individual shots for each FOV. A
11 local flame temperature T_f is defined as the instantaneous temperature at the flame front.
12 Deviations of temperature relative to the instantaneous local flame temperature are defined
13 along the normal coordinate n , as $T'_f = T - T_f$, with corresponding mean and rms values,
14 $\langle T_f \rangle$ and $\langle T'_f \rangle$, respectively.

15 The 2D temperature gradients $\nabla T = \frac{dT}{dr} \mathbf{i} + \frac{dT}{dz} \mathbf{k}$ are determined via first order central
16 differencing after filtering. The gradients of the temperature fluctuations are defined as
17 $\nabla T' = \nabla(T - \langle T \rangle)$. In previous line measurements [11], the 3D temperature gradients
18 throughout the flame were assumed to be parallel to the flame normal obtained from the cross
19 planar OH PLIF measurements. Here we assess the quality of this assumption in 2D by
20 determining the statistics of the angle θ between the temperature and OH gradients as a
21 function of temperature. Further, the characteristic 2D thermal diffusion width, λ_D , of the
22 dissipation layer is obtained from the images. The diffusion width is defined as the full width
23 at 20% of the local maximum temperature gradient, as determined along the direction normal
24 to the layer, which provides a more direct measure of the structure length scale than is
25 possible with 1D measurements [24]. The value of the thermal diffusivity, α , is obtained by

1 interpolating a lookup table of calculated values as a function of temperature from premixed
2 unstrained flames at premixed conditions of $\phi=0.75$.

3

4 **4. Results and discussion**

5

6 **4.1. Single shot measurements**

7 Single shot images of OH PLIF signal, temperature and respective fluctuations for both
8 flow conditions at the regions nearest to the base, FOV1 (bottom panel), and furthest away,
9 FOV3 (top panel), are shown in Fig. 3. For the non-swirling case, SwB1, a comparison of the
10 temperature and OH PLIF images shows that the overall topologies of the OH-PLIF images
11 are well aligned with the temperature images, even in the furthest downstream regions where
12 turbulence is more developed. The flame front contour (location of the highest gradient OH
13 signal) overlaps almost exactly with an isotherm at approximately 1450 K throughout the
14 flame region, with a thermal thickness that is only slightly larger than the laminar flame
15 thickness of $\delta_L = 588 \mu\text{m}$ calculated for $\phi=0.75$.

16 Contrast this behavior with the swirling case, SwB3 (Fig. 3, right), in which the pre-
17 heating region is highly disrupted and convoluted, particularly in the region further
18 downstream (FOV3): regions of high temperature appear in the reactant region, which could
19 be a result of out-of-plane motion of neighboring regions of the flame, as well as entrainment
20 of the flame structures into the reaction zone. The product temperatures are lower than in
21 SwB1 as a result of the swirl-induced entrainment of co-flow air into the central product zone
22 [11] [28]. The OH PLIF signal boundary and the corresponding flame contour is significantly
23 distorted but not dispersed throughout the pre-heating zone. Although the OH radical is not a
24 definitive marker of the flame location under all conditions, the distribution of the OH PLIF

1 signal is very different from that of the temperature. For temperatures above 1200 K, there
2 are no clearly detectable thermal structures.

3 The third row in each panel of Fig. 3 shows the instantaneous fluctuation, T' , relative to
4 the local mean temperature for the two regions FOV 1 and FOV 3. The highest deviations
5 from the mean temperature straddle the location of the flame, as expected.

6

7 **4.2. Flame temperature statistics**

8 Figure 4 shows ensemble mean temperatures and rms fluctuations along the coordinate
9 normal to the flame, n , where $n=0$ is the flame front defined as the location of maximum
10 gradient in the OH LIF signal. The variance is lowest at $n=0$, increases to a maximum away
11 from the flame front, and eventually decreases to zero in the products and reactants. Laminar
12 unstrained premixed flame simulations at $\phi=0.75$ (based on GRI Mech 3.0 [33] and full
13 transport properties) are also shown. The measured maximum conditional mean temperatures
14 in the present dataset appear to be systematically lower than the calculated adiabatic flame
15 temperature (which agrees well with the line measurements in [11]), by 150 K in the non-
16 swirl case. The sources of the discrepancies are unclear, as all calibrations and procedures
17 have been checked.

18 The mean product temperature in the swirling case SwB3 is lower than the corresponding
19 non-swirling case SwB1 owing to entrainment. The fluctuation in temperature is significantly
20 increased by the addition of swirl, particularly in the pre-flame region, due to entrainment of
21 air, both around the outer edges of the flame, as well as through the top in the open
22 recirculation zone [11] [28]. The low fluctuation in temperature at the flame front shows that
23 the location of peak OH gradient, and presumably the reaction zone, is tied to a particular
24 temperature, indicating that the flames appear as curved and strained flamelets.

25

1 ***4.3. Temperature and OH 2D gradient alignment***

2 Since temperature and OH are the most easily imaged scalars, these are often used as
3 surrogates for progress of reaction markers [13] [14] [27] [34]. However, it is clear that their
4 behaviour in the present flames can be very different, and that isocontours of temperature do
5 not always align with those of OH LIF signals. In the present study, it is possible to identify,
6 in 2D, how well the isoscalars align around the flame. In particular, in the study using line
7 measurements [11], two-plane OH LIF imaging was used to determine the orientation of the
8 3D flame normal for the flame crossing the measurement line. This orientation was then used
9 to correct the temperature gradient along the measurement line, under the assumption that the
10 OH contour is parallel to the temperature contour in the vicinity of the thermal zone. Figure 5
11 shows how well this assumption holds by evaluating the angle between the normal directions
12 for contours of temperature and OH LIF signal as a function of the flame distance from the
13 flame along its normal divided by the laminar flame thickness, n/δ_L . Near the flame front
14 contour at $n/\delta_L=0$, θ is approximately zero, indicating that the temperature gradients are well
15 aligned with the OH LIF gradients. At distances beyond $\delta_L/2$, the assumption starts to break
16 down as the angle increases.

17

18 ***4.4. Thermal dissipation scales***

19 The propagation of reactions in a flame depends on the effective generation and
20 dissipation of turbulent structures throughout the flame [5] [6], allowing the increase in the
21 mean rate of reaction throughout the flame. The distribution and characteristic width of the
22 structures generally follow that of a passive scalar, but are significantly affected by the local
23 temperatures, which increase the diffusivity and viscosity, thus suppressing turbulence, and
24 increasing length scales. This has been shown to be true in diffusion flames [23] [24]; here
25 we demonstrate the similarities and differences for swirling premixed flames.

1 Instantaneous images of the thermal dissipation structures are shown in Fig. 6: for the
2 non-swirling case (left), the structures are associated primarily with the flame, and evolve
3 slowly as the turbulence develops downstream. For the high swirl case, the structures are
4 widely distributed, owing to the higher turbulence and entrainment of outside air. Yet these
5 structures become thicker towards the product region (towards the right of each image).

6 In Figure 7, the dissipation structures are characterized by considering the probability
7 density functions (pdf) of their width, λ_D , as a function of the temperature across the flames.
8 The pdfs are conditioned to the temperature of the structure, so that the modes are not
9 representative of the overall image, as the integral of each pdf in Fig. 7 is unity. In general,
10 the structures become systematically thicker towards the high temperature regions, owing to
11 the combined effects of dilatation and increasing viscosity with temperature. Beyond 1400 K,
12 detectable structure widths are mostly a result of the noise remaining from the beam steering
13 correction. For the non-swirling flame SwB1, the most probable width of 600 μm appears at
14 1000 K and corresponds closely to the unstrained laminar flame thickness of 588 μm . For the
15 high swirl case SwB3, the PDF of layer widths has a peak around 300 μm at 400 K, arising
16 from the mixing of product and fresh reactants via entrainment. Less frequent, thicker flame
17 structures appear as temperature increases, to values approximating the width of the
18 unstrained laminar flame, as in case SwB1. In case SwB3, the width of the PDF distributions
19 increases with temperature, and the overall unconditioned PDF distribution is significantly
20 broader than in the non-swirl case.

21 Turbulent combustion models rely on the relationship between statistical variances of the
22 gradients of the reaction progress variable that represents micromixing and the average
23 reaction rate. DNS studies have been used to scale and adjust models based on such
24 correlations [5] [6] [7] [8]. Previous models for scalar dissipation suggest a linear
25 correlation between the Favre mean scalar dissipation of the reaction progress variable, $\tilde{\chi}_c$,

1 and the variance of the relevant progress variable, \tilde{c}'' . Specifically, the work by Kolla *et al.*
 2 [30] and references therein based on the original Bray model [35] suggest a specific
 3 correlation for the normalized Favre averaged scalar dissipation of a reaction progress
 4 variable to its variance, with a coefficient of order unity in the ideal case of high Da. Using
 5 temperature as the progress of reaction, normalized by ΔT , the temperature rise for the
 6 adiabatic flame (1622 K for $\phi=0.75$), it is possible to reproduce these quantities (Fig. 8) in
 7 the form of the normalized Favre averaged scalar dissipation $\hat{\chi}_c = \tilde{\chi}_T \tau_f = \frac{\tau_f}{\Delta T \bar{\rho}} <$
 8 $\rho \alpha |\nabla T''|^2$, where $\tau_f = \frac{\delta_L}{S_L}$ is the laminar flame transit time. The laminar flame transit
 9 time and the density were estimated from the temperature measurements, but variations in
 10 mixture composition were neglected. Values for $\hat{\chi}_c$ are plotted as a function of the Favre
 11 averaged normalized variance in temperature as progress of reaction, $\tilde{c}''^2 = \tilde{T}''^2 / \Delta T^2 =$
 12 $\langle (\rho/\bar{\rho}) (T - \tilde{T})^2 \rangle / \Delta T^2$, and colored by the local mean temperature $\langle T \rangle$.

13 The plots in Fig. 8 for FOV1 and FOV2 of SwB1 show two branches, corresponding to
 14 the higher and lower temperature regions of the flame, reflecting the temperature dependence
 15 of the thermal diffusivity. Further away from the base, additional turbulence is generated by
 16 shear at the edges, the slope becomes lower, and the two branches merge. At this limit, the
 17 mean scalar dissipation rate becomes highly correlated with the mean variance in a nearly
 18 linear relationship, indicating that the variations in molecular diffusivity have less of an
 19 influence. The theory and DNS predictions for the relevant constant suggest that the slope of
 20 the curve should scale as [30]:

$$\hat{\chi}_c = \frac{1}{\beta} \left[\left(2 \frac{K_c^*}{\theta_T} - C_4 (1 + Ka)^{-0.4} \right) \theta_T + C_3 (1 + Ka^{-0.5})^{-1} Da^{-1} \right] \tilde{c}''^2$$

21 where θ_T is the ratio of absolute product to reactant temperatures, $Da = \tau_T / \tau_f$ is the
 22 Dahmköhler number and $Ka = \tau_f / \tau_\eta$ the Karlovitz number, τ_T the integral turbulent time

1 scales, τ_η the Kolmogorov time scale, and the remaining quantities are constants. The values
2 of the constants proposed by Kolla *et al.* [30] are approximately $\frac{K_c^*}{\theta_T} = 0.82$ to 0.85, $C_4 =$
3 1.1 , $C_3 = 1.1$ and $\beta = 6.7$, and values for the present mixture are: $\theta_T = 1 + \frac{\Delta T}{T_0} = 6.5$. In the
4 limit of Da and zero Ka, the slope indicated by the model should be 0.53 to 0.58. Higher
5 values of turbulence would in general decrease Da and increase Ka. The measured slopes for
6 SwB3 are closer to the limit model than those of SwB1, with the closest agreement at
7 location FOV3. The higher turbulence levels in SwB3 and at FOV3 are consistent with the
8 closer match to the theory. On the other hand, for SwB3 there is significant entrainment and
9 mixing, so that one would expect a departure between the correlation between variance and
10 dissipation. Further work connecting the present measurements to local turbulent velocity
11 measurements should enlighten the correlation between theory, experiments and correlations
12 extracted from DNS calculations.

13
14

15 **Conclusions**

16 The present investigation showed how swirl and the ensuing high turbulence and
17 entrainment significantly disrupt the flame thermal zone in a premixed flame, whilst the high
18 temperature reaction zone interface, as marked by the OH contour, remains relatively intact.
19 The temperature at which the maximum OH gradient appears remains relatively unchanged,
20 showing the lowest variance across the flame region, and coinciding with an isocontour of
21 about 1450 K. In support of previous assumptions regarding the alignment of OH and
22 temperature contours, the present experiments showed that indeed, the 2D gradients of OH
23 and temperature align well, up to a distance of about one half the laminar flame thickness
24 away from the flame front, with significant deviations beyond that region in the case of
25 swirling flames.

1 Similarly to previous investigations of diffusion flames, characteristic diffusive widths of
2 the observed thermal structures vary from 300 to 600 microns, from the non-reacting to the
3 higher temperature regions, as a consequence of dilatation and increasing viscosity. The most
4 probable structure widths coincide with the laminar flame thickness in the unswirled, whilst a
5 more uniform distribution of widths appears in the latter case, with a peak at around 400 K
6 temperatures, corresponding to mixing of product and fresh reactants.

7 The Favre-averaged 2D scalar dissipation obtained from the temperature gradients
8 correlates well with the measured variance in the high turbulence regions. In the low
9 turbulence region near the base, the value of the scalar dissipation is not monotonic with the
10 variance of the progress variable and the local temperature. Future work should target
11 understanding the details of these correlations based on the local turbulent velocity
12 characteristics.

13

14

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Figure Captions

Figure 1. Left half: schematic indicating FOV locations for distances above the burner surface. Streamlines and absolute velocity for SwB1 (left half) and SwB3 (right half). Rectangles represent the imaging locations [28].

Figure 2. An example of flame normal extracted from single shot profiles of OH-PLIF. (a) Instantaneous image of normalized OH LIF intensity, (b) temperature field (in K), overlaid with the flame front at the maximum gradient location (black line) and corresponding flame normal (white lines).

Figure 3. Single shot images of normalized OH LIF signal (top rows), temperature (middle rows) in K, and temperature fluctuation, T' , relative to the ensemble averaged temperature field, in K (bottom row) for no swirl (left) and high swirl (right). Top panel: FOV3, bottom: FOV1.

Figure 4: Mean (blue line) and rms (blue bars) fluctuation profiles of the temperature, for FOV1-3 along the normal coordinate n , where zero is the flame front. Black lines denote the unstrained laminar flame values for $\phi = 0.75$.

Figure 5. Scatter plot of normalized angle (in multiples of π) between the normal directions for contours of temperature and OH as a function of the absolute value of the normalized distance from the flame front, coloured by a temperature index defined as $\Omega = (T - T_o)/(T_{f,0} - T_o)$, where $T_{f,0}$ represents the unstrained laminar flame temperature at the location of maximum gradient of OH at equivalence ratio of 0.75. Magenta lines represent the mean and rms values.

Figure 6. Instantaneous temperature fluctuation gradients for SwB1 and SwB3. Bottom to top: FOV1 to 3. The right hand side of the figure is the product side.

Figure 7. Conditioned probability density functions of λ_D widths conditioned on temperature over a 20 K range.

Figure 8. Scatter plots of normalized Favre-averaged scalar dissipation rate, $\tilde{\chi}_c$, and mean Favre variance of progress variable temperature variance, $\widetilde{c''^2}$, colored by the corresponding mean local temperature. The SDR is normalized by the term (δ_L/S_L) ; where S_L is the laminar flame speed of the methane/air flame ($S_L = 0.214$ m/s) and δ_L is the laminar flame thickness ($\delta_L = 0.588$ mm) derived from laminar flame calculations at an equivalence ratio of $\phi = 0.75$. The figures quoted on each panel are the slopes of each correlation.

Table Captions

Table 1. Operating conditions. The velocity of the inner channel is $U_i = 8.3$ m/s ($Re_i = 5960$) and for the outer channel, $U_o = 18.7$ m/s, ($Re_i = 11500$ based on hydraulic diameter of the outer annulus) with co-flow velocity $U_{co} = 0.4$ m/s. Coordinates of the center of the FOV in radial and axial distances from the centreline at the base of the burner, in mm. SFR: ratio of incoming tangential to total flow rate.

Table 2. Maximum value of the ratio for the total mean velocity fluctuation U' divided by the laminar speed S_L for a given axial location, z . Turbulent velocity measurements acquired with laser Doppler anemometry (LDA) and particle image velocimetry (PIV) by Zhou *et al.* [28].

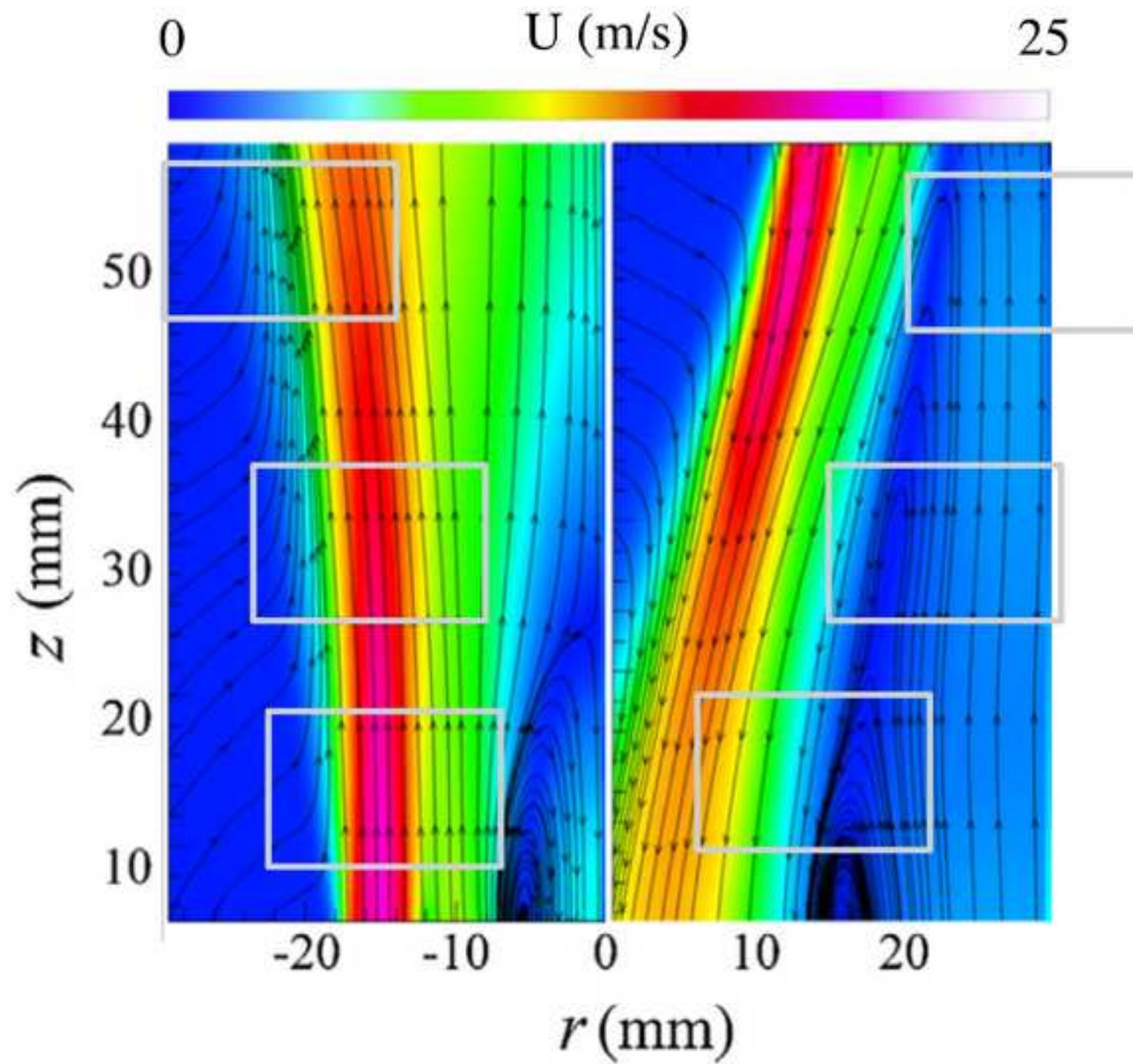
Case	SFR (%)	S (-)	FOV 1	FOV 2	FOV 3
<i>SwB1</i>	0	0.03	(05, 15)	(08, 30)	(11, 50)
<i>SwB3</i>	33	0.54	(13, 15)	(21, 30)	(27, 50)

Table

Flames	$\frac{U'}{S_L}$			
z (mm)	2	10	30	50
<i>SwB1</i>	11.5	9.7	10.0	9.8
<i>SwB3</i>	31.8	27.5	17.9	12.9

*Figure

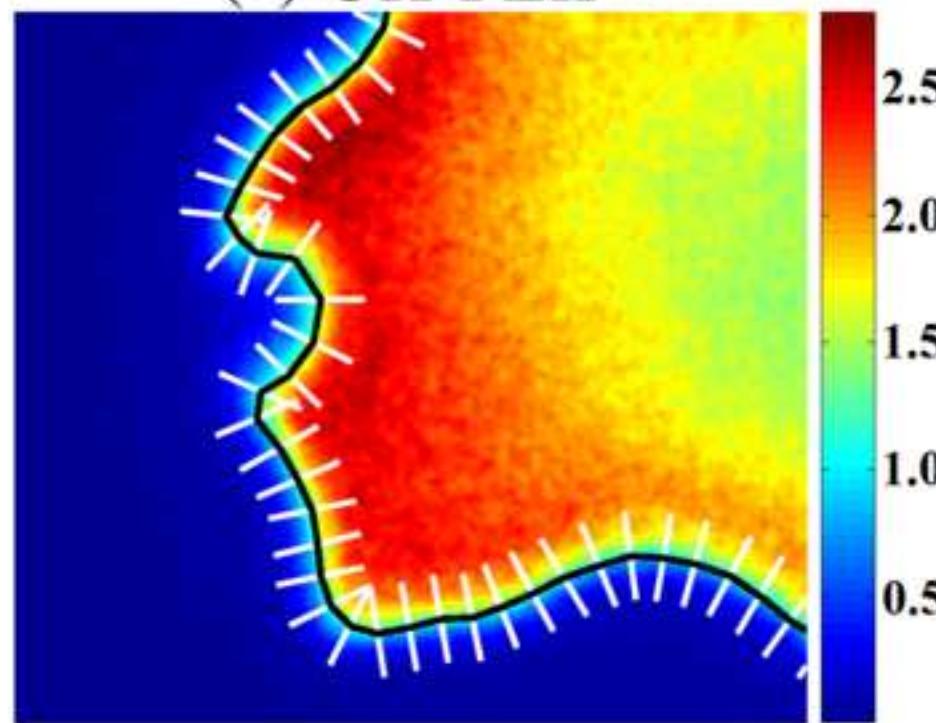
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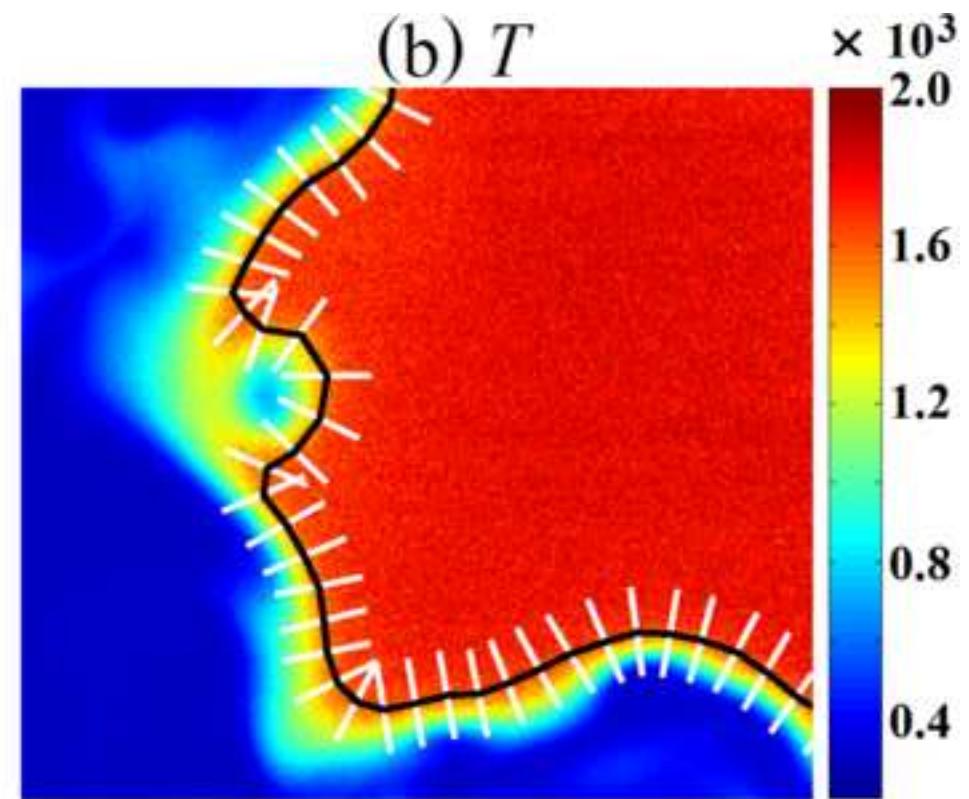
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(a) OH-PLIF

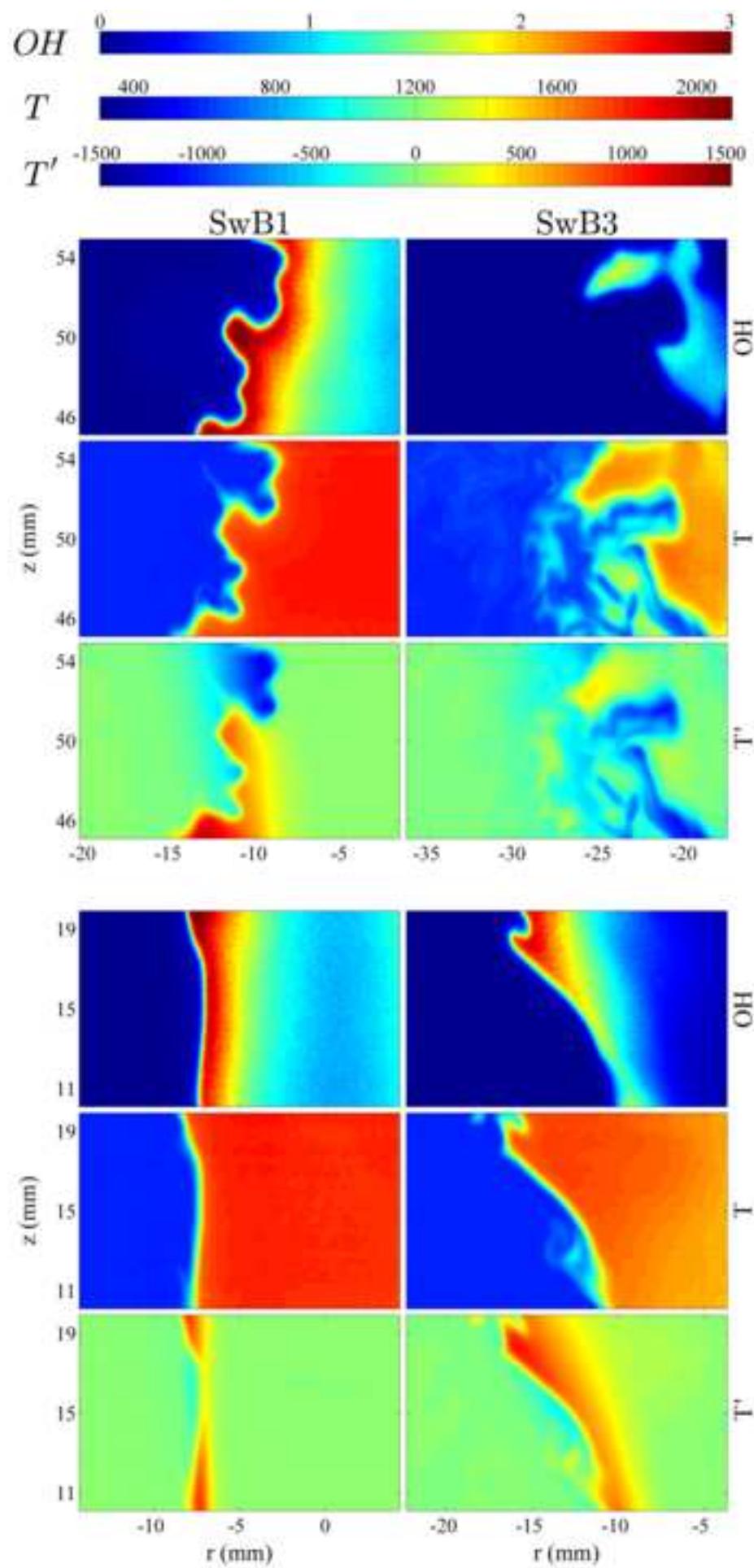


(b) T



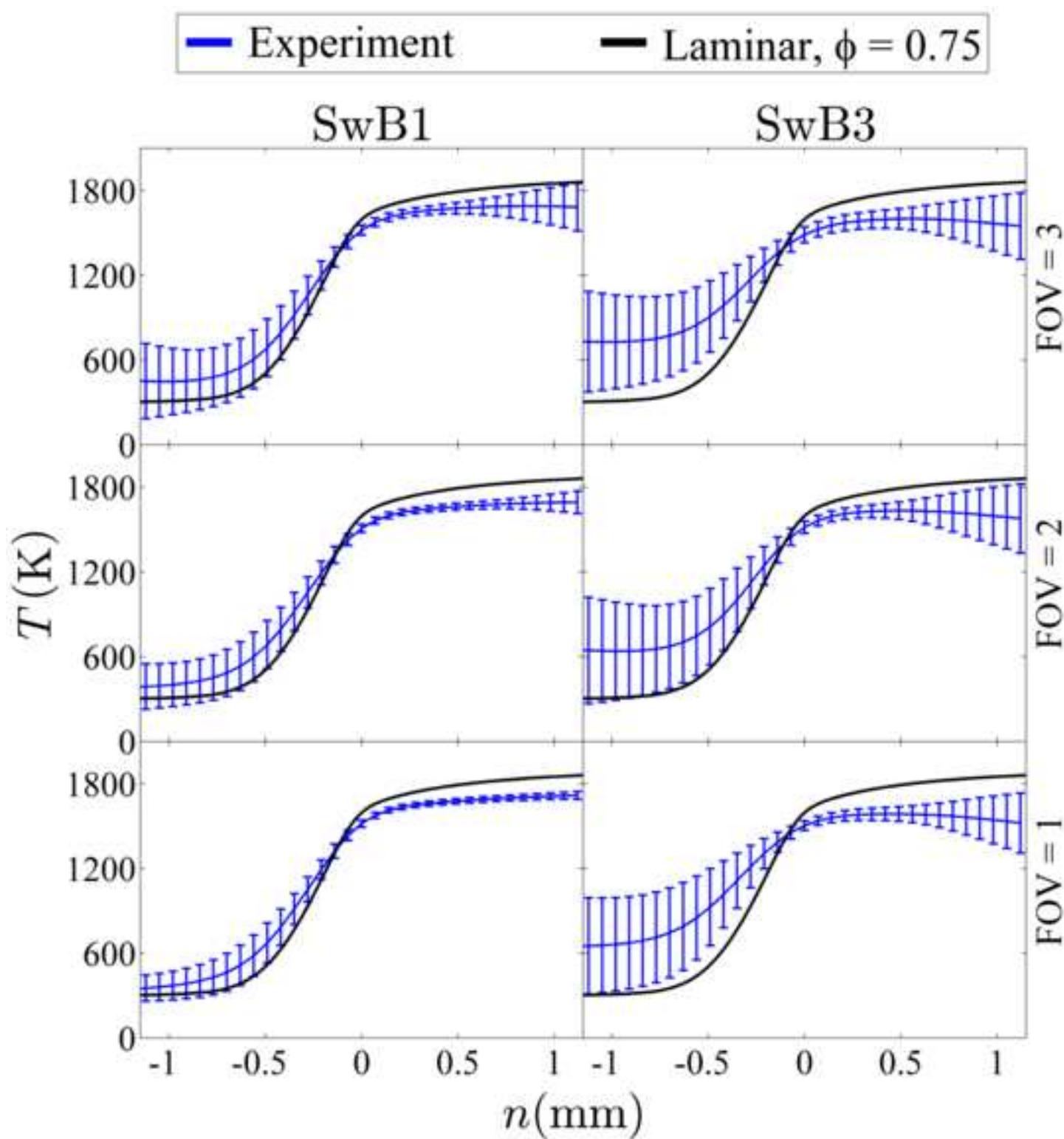
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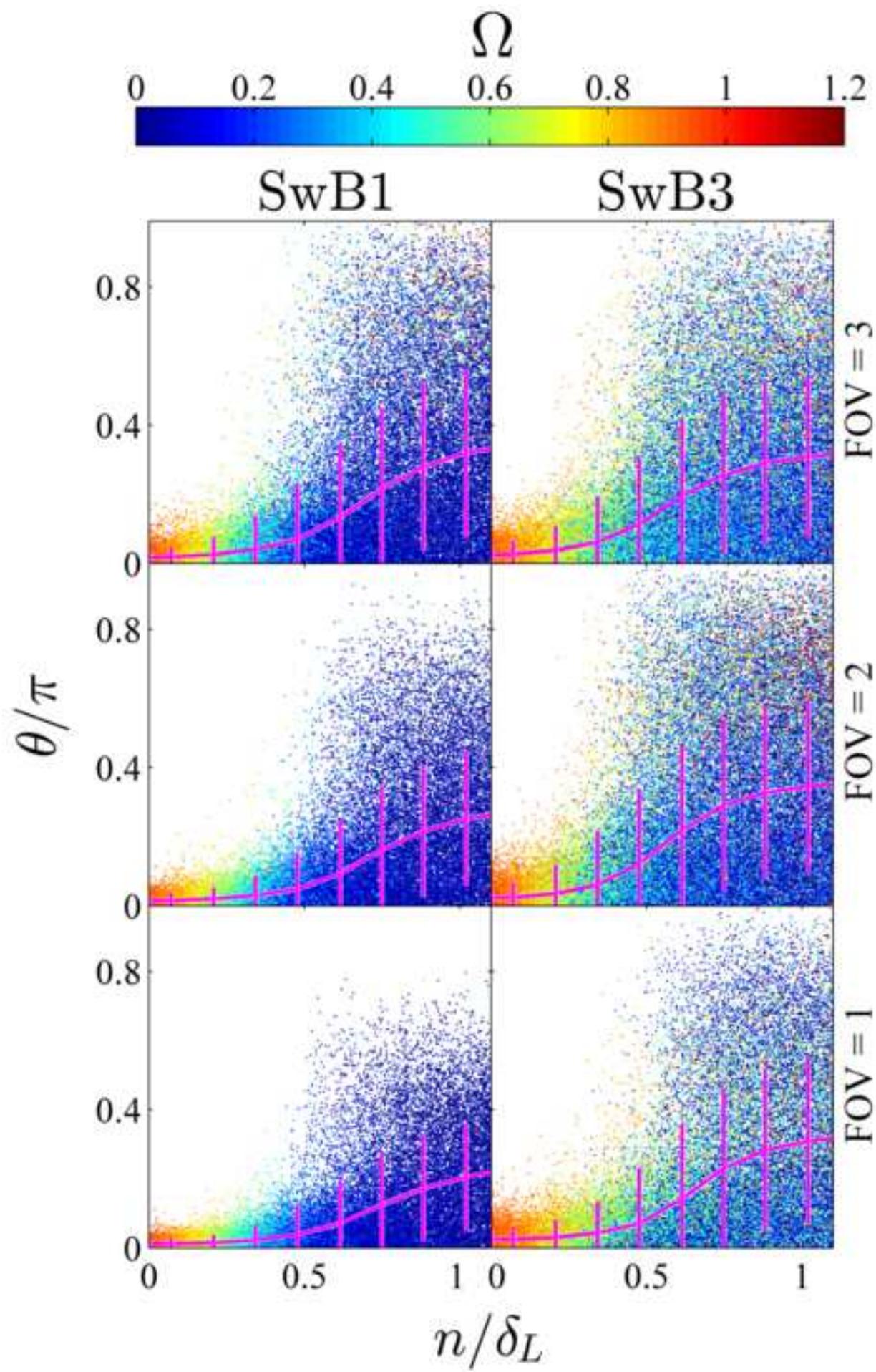
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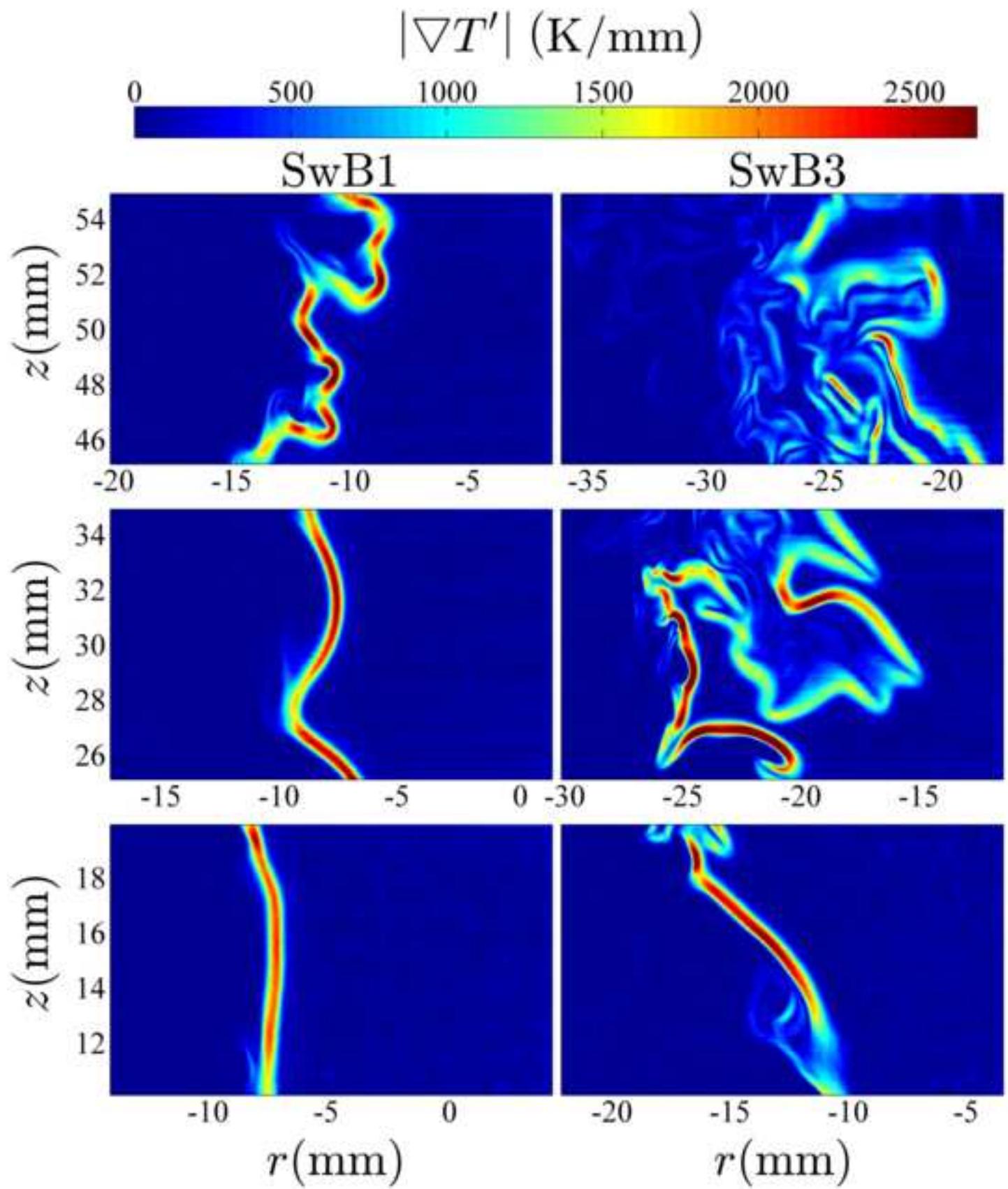
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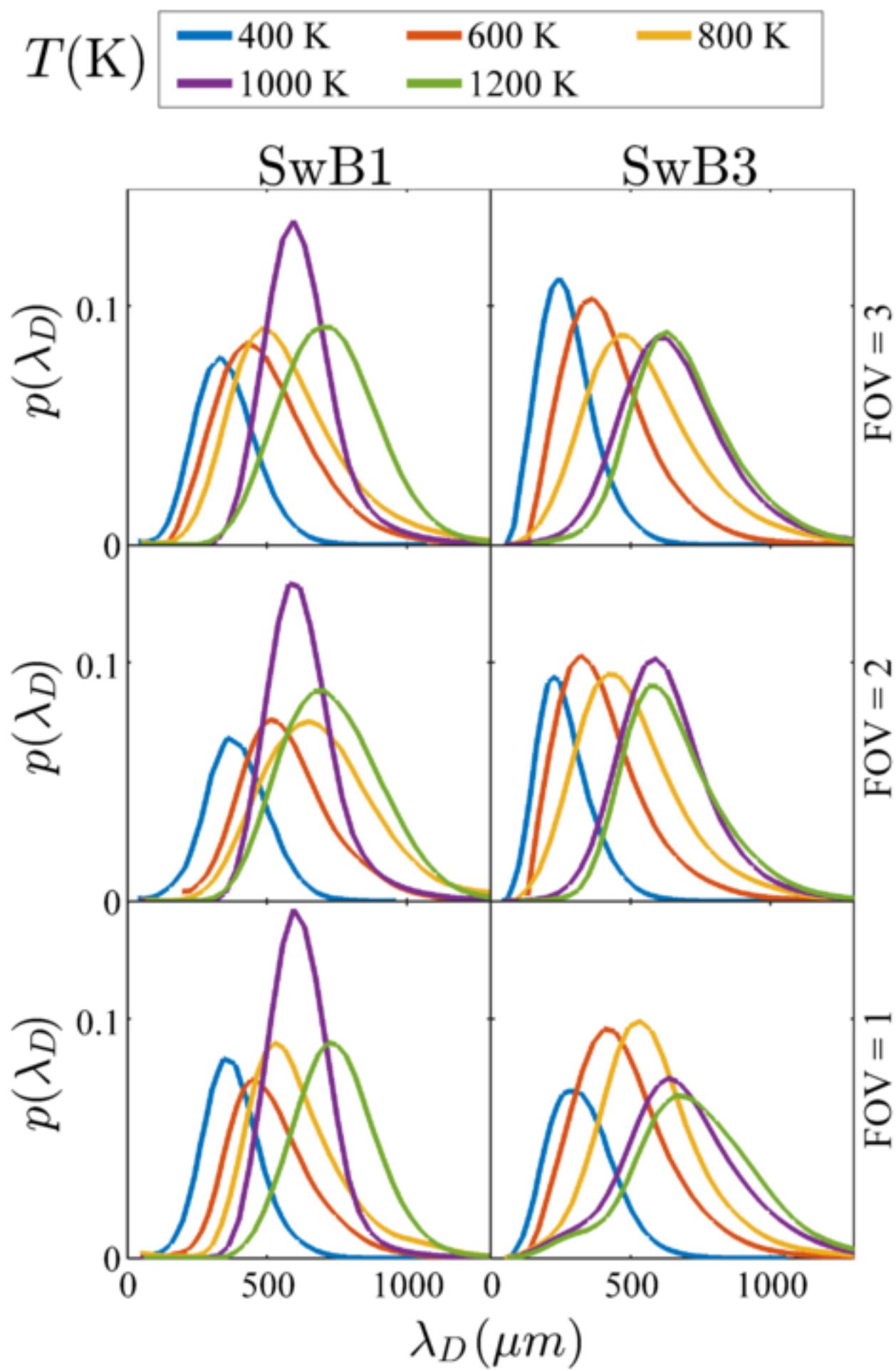
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