

Reversible and selective interconversion of hydrogen and carbon dioxide into formate by a semi-artificial formate hydrogenlyase mimic

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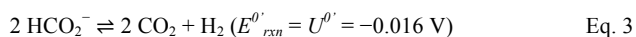
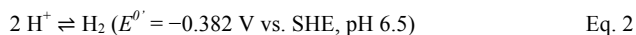
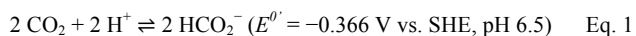
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Supporting Information Placeholder

ABSTRACT: The biological formate hydrogenlyase (FHL) complex links a formate dehydrogenase (FDH) to a hydrogenase (H₂ase) and produces H₂ and CO₂ from formate via mixed-acid fermentation in *Escherichia coli*. Here, we describe an electrochemical and a colloidal semi-artificial FHL system that consists of an FDH and a H₂ase immobilized on conductive indium tin oxide (ITO) as an electron relay. These *in vitro* systems benefit from the efficient wiring of a highly active enzyme pair and allow for the reversible conversion of formate to H₂ and CO₂ under ambient temperature and pressure. The hybrid systems provide a template for the design of synthetic catalysts and surpass the FHL complex *in vivo* by storing and releasing H₂ on demand by interconverting CO₂/H₂ and formate with minimal bias in either direction.

Semi-artificial catalytic systems combine synthetic and biological units to drive challenging reactions and provide new concepts for catalyst design.¹ Such solar-driven systems have already demonstrated coupling of water oxidation to the production of fuels (reduction of protons and CO₂).²⁻⁵ However, storage and transport of energy vectors are also important components in energy production-utilization cycles and their development will benefit from more advanced concepts and model systems.

H₂ is a promising fuel and its storage in formate allows for easier storage and transport; H₂ and formate are therefore an attractive energy vector pair. Furthermore, H₂ gas cleanly separates from dissolved formate, and their interconversion comes at little thermodynamic cost (Eq. 1-3).^{6,7} However, achieving kinetic efficiency in HCO₂⁻/H₂ interconversion remains a synthetic challenge. Artificial systems commonly compete between decomposition of formic acid to CO and H₂O (dehydration), and CO₂ and H₂ (dehydrogenation), and rely on precious metals, high temperature/pressure, organic solvents and light.⁸⁻¹⁰



FHL complexes are biological machines for HCO₂⁻/H₂ interconversion¹¹ that are either membrane-associated complexes composed of a multisubunit [NiFe]-H₂ase coupled to a FDH,¹¹⁻¹³ or

smaller soluble complexes of an [FeFe]-H₂ase and an FDH.^{14,15} The *Escherichia coli* FHL-1 complex, composed of the membrane-bound [NiFe]-H₂ase 3 (HYD-3/HycE) and FDH-H (FdhF; Figure 1a) represents a well-studied FHL, evolving H₂ under fermentative conditions.^{11,12} The constituent enzymatic units of FHL-1 have been demonstrated to be reversible electrocatalysts,¹⁶⁻²⁰ but the complex is catalytically biased toward H₂ production from formate.^{14,15,19} Interconversion of HCO₂⁻/H₂ has also been reported in whole-cell studies,^{14,20} notably in sulfate-reducing bacteria in the absence of sulfate.^{21,22} *Desulfovibrio vulgaris* Hildenborough can grow by converting formate to H₂,²³ with formate oxidation catalyzed by a periplasmic FDH, and H₂ produced either via a direct pathway (periplasmic H₂ase) or via transmembrane electron transfer (cytoplasmic H₂ase).²⁴

Redox biocatalysts, including H₂ases and FDHs, have been coupled to other enzymatic processes via electron relays. H₂ases have been connected to nitrate and fumarate reductases,²⁵ diaphorase modules,²⁶ nicotinamide reductase and alcohol dehydrogenase²⁷ via graphitic particles. Coupling a H₂ase to carbon monoxide dehydrogenase efficiently catalyzed the water-gas shift reaction.²⁸ Enzymatic cascades have linked FDH with formaldehyde and alcohol dehydrogenases for methanol production.^{29,30} However, the reversible interconversion of substrate and product has not been previously accomplished with such coupled enzymes *in vitro*.

Here, a semi-artificial FHL complex mimic is presented by re-wiring FDH^{31,32} and H₂ase³³ from *D. vulgaris* Hildenborough into electrochemical and colloidal systems (Figure 1b,c). These systems rely on efficient electrical contact of the [W/Se]-FDH active-site via four [Fe₄S₄] clusters and the [NiFeSe]-H₂ase active-site via three [Fe₄S₄] clusters with nanostructured ITO.

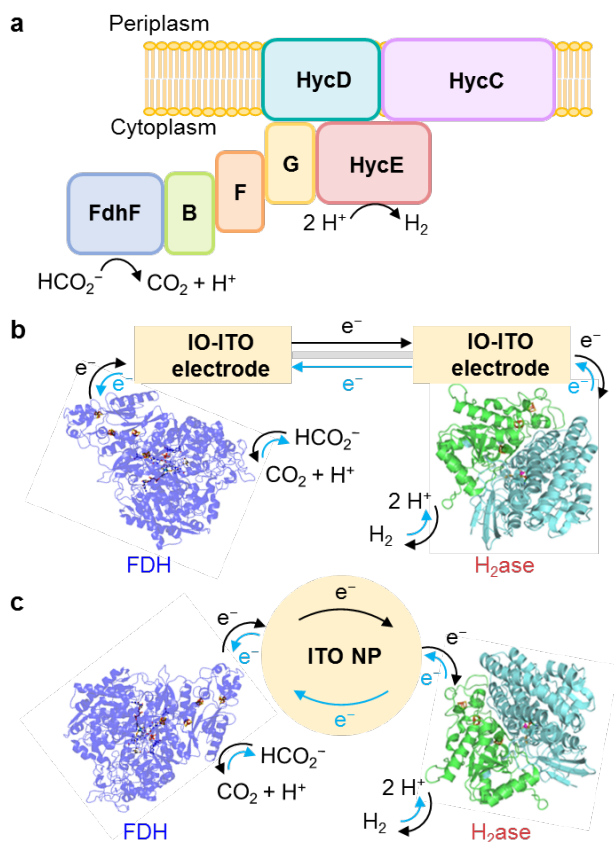


Figure 1. (a) Biological *E. coli* FHL-1 complex. FdhF, [Mo]-FDH; B/F/G, Fe-S cluster-containing proteins; HycE, [NiFe]-H₂ase; HycD/C, membrane proteins.¹⁷ (b) IO-ITO|FDH||IO-ITO|H₂ase cell: IO-ITO|FDH wired to IO-ITO|H₂ase electrode. (c) FDH-ITO-H₂ase nanoparticle (NP) system with enzymes immobilized onto ITO NP in solution. Species size not drawn to scale.

Macro-mesoporous inverse opal (IO) ITO electrodes (20 μm film thickness; 0.25 cm^2 geometrical surface area) were assembled as previously reported.³⁴ IO-ITO|FDH and IO-ITO|H₂ase electrodes were prepared by drop-casting an FDH solution (2 μL , 19 μM with 50 mM DL-dithiothreitol, incubated for 15 min) and a H₂ase solution (2 μL , 5 μM), onto IO-ITO.^{31,34} Protein film voltammetry (PFV) was recorded using a three-electrode configuration (Figure 2a and S1) in CO₂/NaHCO₃ solution. Current densities (J) of $-185 \mu\text{A cm}^{-2}$ (CO₂ reduction to formate by FDH) and $-450 \mu\text{A cm}^{-2}$ (H⁺ reduction to H₂ by H₂ase) were observed at an applied potential (E_{app}) of -0.6 V vs. standard hydrogen electrode (SHE). Addition of sodium formate (20 mM) to the IO-ITO|FDH system resulted in formate oxidation to CO₂ and $300 \mu\text{A cm}^{-2}$ was reached at -0.2 V vs. SHE. After purging the IO-ITO|H₂ase system with H₂ (0.4 bar), H₂ oxidation to H⁺ was observed and $440 \mu\text{A cm}^{-2}$ was reached at -0.2 V vs. SHE. The voltammograms cut through zero current around the formal redox potentials (Eq. 1,2), demonstrating reversible electrocatalysis for both enzymes.^{6,35}

Multiple PFV scans of IO-ITO|FDH and IO-ITO|H₂ase (Figure S2) showed minimal desorption/activity losses. Controlled-potential electrolysis (CPE) of IO-ITO|FDH and IO-ITO|H₂ase was performed to measure H⁺/CO₂ reduction ($E_{\text{app}} = -0.6 \text{ V}$) as well as H₂/formate oxidation ($E_{\text{app}} = -0.2 \text{ V}$) (Figure S3). Both electrodes retaining $>90\%$ of the initial current after 24 h in both directions. Faradaic efficiencies (η_{F}) for formate and H₂ production were determined to be 76 and 77%, respectively. Efficiency losses may be attributed to capacitive background current of porous IO-ITO,³⁴ undetected trapped product and a contribution from ITO/FTO degradation.^{36,37}

The comparable formal redox potentials of H⁺/H₂ and CO₂/HCO₂⁻ conversion (Eq. 1-3), reversible catalysis of the individual enzymes, high and matching current densities, and good stability make this enzyme pair a promising candidate for assembling a reversible HCO₂⁻/H₂ interconversion system.⁶ Thus, the IO-ITO|FDH (working electrode) was wired to the IO-ITO|H₂ase (counter electrode) in a two-electrode configuration (Figure 2b). When no additional substrate was present (only buffering CO₂ and H⁺), only a non-catalytic (capacitive) current was observed. Upon addition of formate, an oxidative current was observed (formate oxidation to CO₂ and H⁺ reduction to H₂) at a positive applied voltage ($U > 0 \text{ V}$); $250 \mu\text{A cm}^{-2}$ was reached at $U = 0.2 \text{ V}$. Addition of H₂ resulted in a reductive current (H₂ oxidation to H⁺ and CO₂ reduction to formate) with $-250 \mu\text{A cm}^{-2}$ obtained at $U = -0.2 \text{ V}$.

To achieve reversible formate/H₂ interconversion (Eq. 3) both formate and H₂ were added in addition to CO₂ and H⁺. A reversible voltammogram was observed, with zero current at approximately U^0 at 0.02 V. A marginally more positive or negative voltage drives the reaction in either direction, demonstrating reversible unbiased electrocatalysis, as opposed to that demonstrated for *E. coli* FHL-1.¹⁹ $200 \mu\text{A cm}^{-2}$ and $-200 \mu\text{A cm}^{-2}$ were reached at $U = 0.2 \text{ V}$ and -0.2 V , respectively. Multiple PFV scans of the IO-ITO|FDH||IO-ITO|H₂ase cell (Figure S4) showed stability of the system with marginal losses. Control experiments with IO-ITO|FDH (or ITO|H₂ase) wired to IO-ITO (Figure S5) gave only a small capacitive current in the presence and absence of substrates.

CPE during 2 h at $U_{\text{app}} = 0.2 \text{ V}$ with the IO-ITO|FDH||IO-ITO|H₂ase cell with formate present (Figure 2c) produced H₂ ($5.84 \pm 0.88 \mu\text{mol cm}^{-2}$) with η_{F} of $(79 \pm 11)\%$. Similarly, CPE at $U_{\text{app}} = -0.2 \text{ V}$ for 2 h with H₂ present generated formate ($5.00 \pm 0.80 \mu\text{mol cm}^{-2}$) with η_{F} of $(81 \pm 15)\%$. This semi-artificial system exhibited good stability, retaining $>95\%$ of its initial activity after 2 h in both directions. After equilibration, the cell exhibited high bidirectional stability for >1 day (Figure S6). For formate oxidation ($U_{\text{app}} = 0.2 \text{ V}$), H₂ ($36.28 \mu\text{mol cm}^{-2}$) was detected with $\eta_{\text{F}} = 72\%$. For H₂ oxidation ($U_{\text{app}} = -0.2 \text{ V}$), formate ($42.80 \mu\text{mol cm}^{-2}$) was detected with $\eta_{\text{F}} = 77\%$. Similarly to the three-electrode systems, capacitive currents and FTO/ITO dissolution^{36,37} might have decreased the product yield.

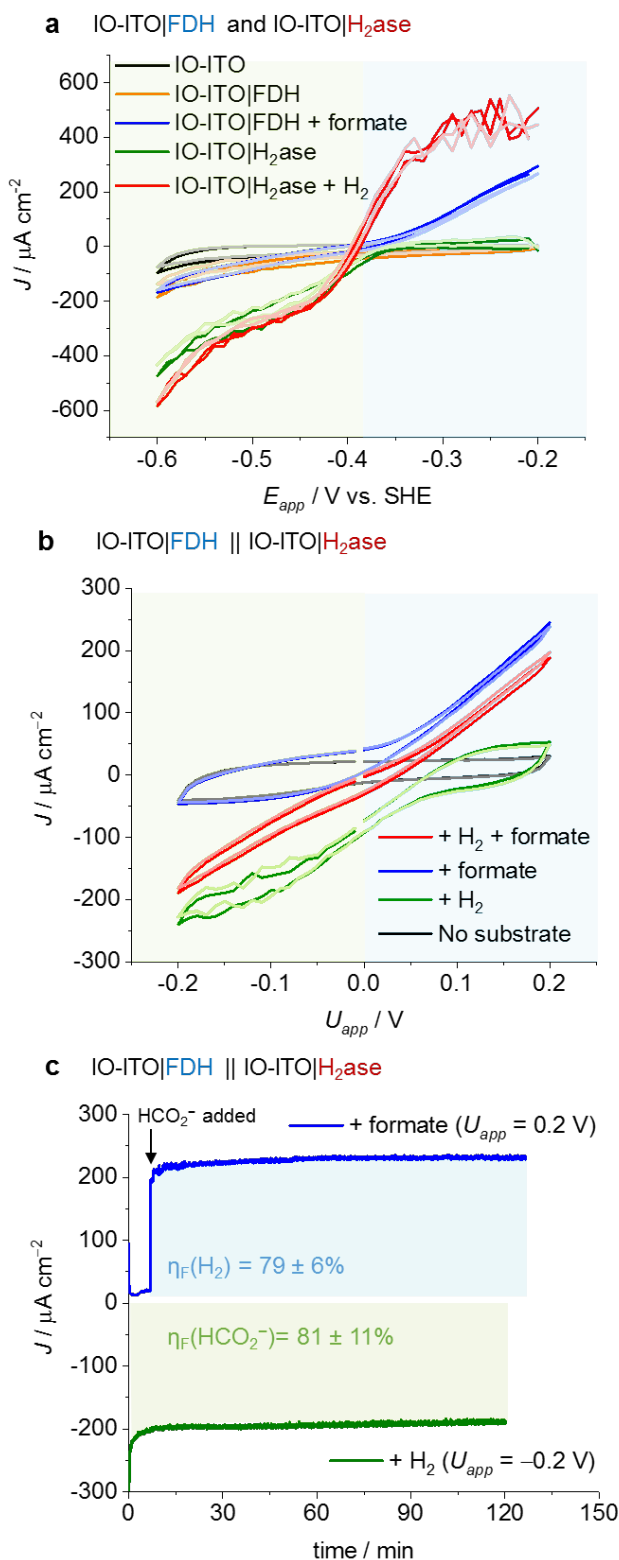


Figure 2. (a) Three-electrode PFV ($v = 5 \text{ mV s}^{-1}$, 1st and 5th scan, increasing transparency) using IO-ITO|FDH or IO-ITO|H₂ase working, Ag/AgCl (KCl_{sat}) reference, Pt counter electrode. (b) Two-electrode PFV ($v = 5 \text{ mV s}^{-1}$, 1st and 5th scan) of IO-ITO|FDH wired to IO-ITO|H₂ase. (c) Two-electrode CPE of IO-ITO|FDH wired to IO-ITO|H₂ase. Conditions: CO₂/NaHCO₃ (100 mM), KCl (50 mM), 1 bar CO₂ or 0.4/0.6 bar H₂/CO₂, pH_{initial} = 6.5–6.7, T = 25 °C, stirring. Substrates: formate (20 mM) and/or 0.4/0.6 bar H₂/CO₂.

To further investigate the system's reversibility without electrochemical wiring, FDH and H₂ase were co-assembled on ITO NPs (0.3 mg mL⁻¹) (Figure 3 and S7) dispersed in solution (see Supporting Information). Solutions of FDH (19 nM, incubated as above) and H₂ase (3.4 nM) were added to the vessel, which was sealed and purged with CO₂. Either formate or H₂ was introduced to the vessel. FDH:H₂ase molar ratios (Figure S8) and total concentrations (Figure S9a,b) were screened for optimum H₂ evolution rate. The optimal system contained an enzyme loading of approximately 40 FDH and 7 H₂ase particles per ITO NP, based on the adsorption surface area of 27 m² g⁻¹, ~31,400 nm² per NP (assuming a 50 nm diameter sphere) and an enzyme footprint of ~100 nm².

Upon formate addition to the FDH–ITO–H₂ase system (Figure 3a), H₂ was produced with a rate (Figure S9c) of $0.24 \pm 0.01 \mu\text{mol H}_2 \text{ h}^{-1}$ during the first 8 h [turnover number, TON = $(23.0 \pm 1.5) \times 10^3$ and turnover frequency, TOF = $6.4 \pm 0.4 \text{ s}^{-1}$ for the H₂ase], after which the rate started to decrease (Table S1). Equilibrium was reached after ~72 h ($5.82 \pm 0.24 \mu\text{mol H}_2$, pH 6.88, T = 23 °C), in agreement with calculations ($5.95 \mu\text{mol}$, 2.97 mM of H₂, see Supporting Information).⁷

In the presence of H₂, the FDH–ITO–H₂ase system (Figure 3b), produced formate with an initial reaction rate of $1.33 \pm 0.01 \mu\text{mol formate h}^{-1}$ [TON = $(15.8 \pm 5.4) \times 10^3$ and TOF = $4.4 \pm 1.5 \text{ s}^{-1}$ for the FDH] for the first 8 h (Figure S9d). Equilibrium was reached after ~96 h ($36.16 \pm 1.47 \mu\text{mol formate}$, pH 6.99, T = 23 °C), consistent with calculations ($37.11 \mu\text{mol}$, 18.56 mM of formate).⁷ Control experiments with no ITO NPs, omitting an enzyme or with denatured enzymes (Figure S10) showed only negligible H₂ and formate production (<0.2 μmol) (Table S2 and S3). Therefore, the ITO NPs act as a semi-heterogeneous electron relay facilitating electron transfer between electroactive FDH and H₂ase.

In *D. vulgaris* cells, the two periplasmic enzymes exchange electrons through the type-I cytochrome *c*₃ (TpIc₃) electron acceptor.²⁴ We therefore studied the activity of these enzymes in solution with TpIc₃. A high concentration of the cytochrome (1.9 μM, 100-fold excess vs FDH) was required to achieve comparable kinetics of H₂ and formate production (Fig. S11a,b), revealing the superiority of co-immobilizing the two enzymes on synthetic ITO to achieve efficient electron transfer.

In summary, we have presented how semi-artificial systems consisting of FDH and H₂ase from *D. vulgaris* wired to ITO can mimic the biological FHL complex. The semi-artificial FHL systems are based on a bottom-up design that employs a pair of reversible redox enzymes immobilized on conductive scaffolds to enable an overall catalytic reaction to proceed to thermodynamic equilibrium. The semi-artificial FHL concept can be deployed in either an electrochemical cell or a self-assembled colloidal suspension, providing versatility for applications in different contexts. The design concept of linking two half-reactions via a conductive scaffold also provides a blueprint to develop improved synthetic H₂/formate cycling catalysts in future development.

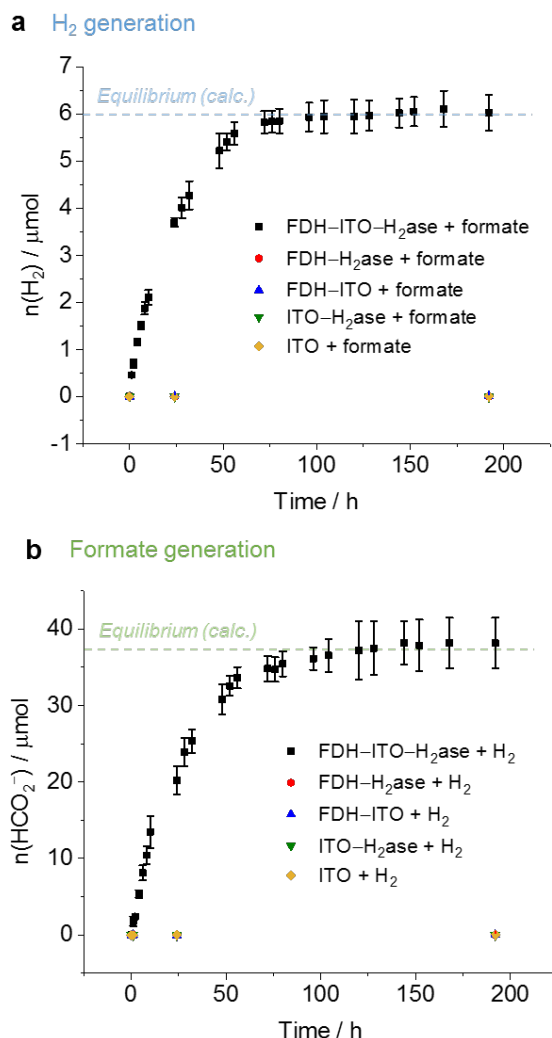


Figure 3. Colloidal FDH-ITO-H₂ase NP system using ITO NPs (0.3 mg mL⁻¹), FDH (19.0 nM) and H₂ase (3.4 nM). (a) H₂ production in the presence of 10 mM formate and 1 bar CO₂. V_{headspace} = 1.72 mL. (b) Formate production in the presence of 0.4/0.6 bar H₂/CO₂. V_{solution} = 2 mL. Conditions: CO₂/NaHCO₃ (100 mM), KCl (50 mM), 1 bar CO₂ or 0.4/0.6 bar H₂/CO₂, pH_{initial} = 6.5–6.7, T = 23 °C, stirring.

ASSOCIATED CONTENT

Supporting Information

Materials, experimental methods, Figures and Tables. This material is available free of charge via the ACS Publications website at <http://pubs.acs.org>.

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Notes

The authors declare no competing interests.

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